

## ORIGINAL ARTICLE

# Chemical modification in and on single phase $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$ nanopowders produces “chocolate chip-like” $\text{Ni}_x@[\text{NiO}]_{0.5-x}[\text{Al}_2\text{O}_3]_{0.5}$ nanocomposite nanopowders

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**Abstract**

Phase-pure  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  spinel nanoparticles (NPs) with limited aggregation were obtained via liquid-feed flame spray pyrolysis (LF-FSP) by combusting metalloorganic precursor solutions. Thereafter “chocolate chip-like”  $\text{Ni}_x@[\text{NiO}]_{0.5-x}[\text{Al}_2\text{O}_3]_{0.5}$  nanoparticles consisting of primary  $[\text{NiO}]_{0.5-x}[\text{Al}_2\text{O}_3]_{0.5}$  particles with average particle sizes of 40–60 nm decorated with Ni metal particles (<10 nm in diameter) dispersed on the surface were synthesized by heat treating the spinel NPs at 800°C/7 h in flowing 5%  $\text{H}_2:\text{N}_2$  100 mL/min in a fluidized bed reactor. The synthesized materials were characterized using TEM, XRD, FTIR, and TGA/DTA. The Ni depleted areas consist primarily of  $\gamma\text{-Al}_2\text{O}_3$ . The Ni content (800°C) was determined by TGA to be  $\approx 11.3$  wt.% based on TGA oxidation behavior. The successful synthesis of such nanocomposites with limited aggregation on a high temperature support provides a facile route to synthesize well-defined NP catalysts. This work serves as a baseline study for an accompanying paper, wherein thin, flexible, dense films made from these same NPs are used as regenerable catalysts for carbon nanotube syntheses.

**KEYWORDS**

liquid feed-flame spray pyrolysis, nanocomposites, nickel aluminate, phase pure spinel nanopowders

## 1 | INTRODUCTION

The search for low-cost, high-performance catalysts for energy-related processes continues to be a research hotspot recently as the world shifts from coal to natural gas energy feedstocks. Thus more and more emphasis has been placed on developing metal catalysts with very high and stable activity and also on exploring materials and methods of replacing precious metals that is, Pt, Pd, Ru with less costly metals while also compensating for lower catalytic activities.<sup>1–6</sup> Compared with precious metals, nickel and other transition metals are relatively more abundant and following appropriate activation can offer high catalytic activity.<sup>7–12</sup> Equally important is the development of high activity catalysts that

maintain their activity with time especially at higher processing temperatures.

In general, the high temperature stability of most metal catalysts is relatively low. It has long been recognized that deactivation pathways often involved sintering (Ostwald ripening) of metal particles on support surfaces. Likewise, the role of support materials in stabilizing catalysts is also well recognized and long studied. In particular,  $\text{Al}_2\text{O}_3$  and  $\text{SiO}_2$  supported nickel-based catalysts are widely used in industry. Such supported non-precious metal catalysts offer the advantages of low cost, wide utility, ease of recovery combined with high activity, selectivity and stability especially for reforming and hydrogenation processes.<sup>13–18</sup>

Conventional preparative methods for these kinds of catalysts typically employ various forms of solution impregnation.<sup>19–22</sup> When the supported metal catalyst is prepared by impregnation, the precursor to the active metal component is affected by support surface tension, chemistries and solvation effects within the impregnation solution, ease of deposition defined by surface wetting as well as the dynamics of drying. Obviously, there are multiple variables controlling the interactions between the precursor metal salts and the support during and after impregnation that defines the extent of surface coverage, potential for precursor crystallization or aggregation during deposition and activation thereafter. Thus, optimizing activity and specific active surface area can sometimes be considered an art-form rather than good science. In this paper, we describe a completely different approach that relies on synthesized high surface area NPs that can be carefully transformed to active catalytic systems without first introducing an impregnation step. In this process, active catalyst nanoparticles are proposed to be generated by chemically modifying the supporting high surface area phase. Our approach begins with the synthesis of high surface area (60 m<sup>2</sup>/g) nickel-containing spinel NPs, [NiO]<sub>0.5</sub>[Al<sub>2</sub>O<sub>3</sub>]<sub>0.5</sub>.

Spinel oxide crystal lattice ions often form with both 2<sup>+</sup> and 3<sup>+</sup> ions found interchangeably in both the tetrahedral and octahedral positions depending on the elements involved and leading to a wide variety of properties.<sup>23–26</sup> Theoretically, transition metal aluminum spinel oxides, especially nickel-containing, offer considerable potential and practical applications as catalysts for such reactions as hydrocarbon cracking, methane- and methanol-steam reforming, and dehydrogenation.<sup>27–32</sup> Alumina supported nickel catalysts are relatively inexpensive compared to other types of catalysts. Therefore, considerable effort has been devoted to exploring and optimizing their properties.<sup>33–36</sup> Perhaps most important is the fact that it is relatively difficult to obtain high surface area spinel-based active catalysts due to the fact that high temperature processing is required simply to produce the spinel structure. Such high temperature processing frequently equates to extensive loss of surface area.

In the current study, the inherent thermal stability provided by a spinel phase allows generation of high surface area nanoparticles that can be reductively modified by exposure to H<sub>2</sub> to decorate the surface of the [NiO]<sub>0.5</sub>[Al<sub>2</sub>O<sub>3</sub>]<sub>0.5</sub> NPs with well dispersed and uniform sized catalytically active nickel metal particles. In principle, this approach may allow one to reduce side reactions caused by sintering (Ostwald ripening) of the active nickel metal particles.

Nickel aluminate spinels have been prepared via many methods including solid-state reaction, ultrasound irradiation-assisted precursor processing, sol-gel processing, and ion exchange in zeolites.<sup>37–42</sup> However, it is very difficult to prepare single-phase, nickel aluminate spinels with high surface areas and controlled stoichiometries. The as-prepared

nickel aluminate spinels still suffer from serious powder agglomeration, uneven particle size distributions, and oversized particles, which affect seriously the application of nickel aluminate spinels in many fields. As a very effective method of generating a wide variety of single and mixed metal oxide NPs from metalloorganic precursors, liquid feed flame spray pyrolysis (LF-FSP) has been employed by many groups.<sup>43–54</sup> Our group typically uses 1–10 wt. % ceramic yield ethanol solutions of metal carboxylates, alkoxides, beta-diketonates, and/or related metalloorganic precursors to prepare a wide variety of single and mixed-metal oxide NPs that provide novel catalyst.<sup>51–53</sup>

As practiced, these precursor solutions are aerosolized with oxygen, combusted at flame temperatures of 800–1200°C in a 1.5 m long quartz or stainless-steel tube to produce a cloud of ions. This cloud of ions is quenched in a time frame of just a few 100 msec to temperatures of 300–400°C. Thus, the solution and then the gas phase composition are usually retained in the resultant NPs.

The “as-shot” NPs are typically agglomerated by not aggregated, making them easy to disperse. They normally exhibit average particle sizes (APSS) of 40–100 nm equated with specific surface areas (SSAs) of 100–20 m<sup>2</sup>/g. The NPs produced can be amorphous or offer simple crystal structures (easiest to form during quenching) this includes phases not normally observed in the phase diagrams of the components as kinetic products formed during the rapid quench. In some examples, core-shell structures or even three-phase NPs form (nanostructured NPs) if all the phases are immiscible.<sup>53</sup>

Early LF-FSP studies sought to develop a picture of the breadth of scope of LF-FSP for NP synthesis. We coincidentally probed NP photophysical finding that rare earth doped δ-Al<sub>2</sub>O<sub>3</sub> NPs exhibit incoherent lasing for example.<sup>55,56</sup> As briefly noted above we also were able to demonstrate novel catalytic properties for a series of core-shell Ce<sub>1-x</sub>Zr<sub>x</sub>O<sub>2</sub>@δ-Al<sub>2</sub>O<sub>3</sub>. Recently we reported on the utility of selected cobalt spinel NPs for the synthesis of carbon nanotubes.<sup>57–59</sup> These results coupled with an interest in using nickel based thin films as catalysts allowed us to demonstrate the potential utility of a thin, flexible ceramic nickel aluminate as a precursor to regenerable catalysts for carbon nanotube syntheses.<sup>60</sup>

Consequently, LF-FSP makes it possible to synthesize a wide variety of mixed-metal oxide NPs with high purity, limited aggregation, with well-controlled stoichiometries, and phase compositions. LF-FSP provides a feasible way to develop novel nickel/nickel aluminate nanocomposites powders and thereafter catalysts, using nickel aluminate spinel NPs as the starting point. To our knowledge there are few related reports that have explored this approach. Furthermore, the work reported here provides a novel structure using nickel aluminate spinel NPs as the functional catalyst carrier for nickel metal, which can enhance the catalytic activity along with the high added value utilization of nickel aluminate spinel NPs.

Besides, nickel aluminate spinel NPs as a functional carrier can be regarded as a source of nickel metal, and the dispersibility of active nickel metal can be improved significantly.

## 2 | EXPERIMENTAL

### 2.1 | Sample preparation

**Precursors.** Alumatrane  $\text{Al}(\text{OCH}_2\text{CH}_2)_3\text{N}$ , was prepared as described elsewhere.<sup>52</sup> Nickel acetate,  $\text{Ni}(\text{O}_2\text{CCH}_3)_2$  was purchased from Sigma Aldrich (Milwaukee, WI) and used as received. Anhydrous ethanol fuel and solvent was purchased from Decon Labs (King of Prussia, PA).

**Nanopowder synthesis.**  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  NPs were synthesized by LF-FSP as reported previously.<sup>53</sup> Alumatrane and nickel acetate were dissolved in EtOH at the selected molar ratio to give a solution with an approximate ceramic yield of 3 wt. %. This precursor solution was aerosolized with oxygen and combusted in a chamber with methane/oxygen torches and shield  $\text{O}_2$ .<sup>53</sup> The NPs were collected downstream in electrostatic precipitators (ESP) operated at a 10 kV direct current potential.

**Fluidized bed reactor (FBR):** As-prepared  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  NPs were placed in a quartz tube reactor and heated at selected temperatures of 500° to 900°C at 10°C/min/7 h in 100 mL/min 5/95  $\text{H}_2:\text{N}_2$  flow Figure 1.

### 2.2 | Materials characterization

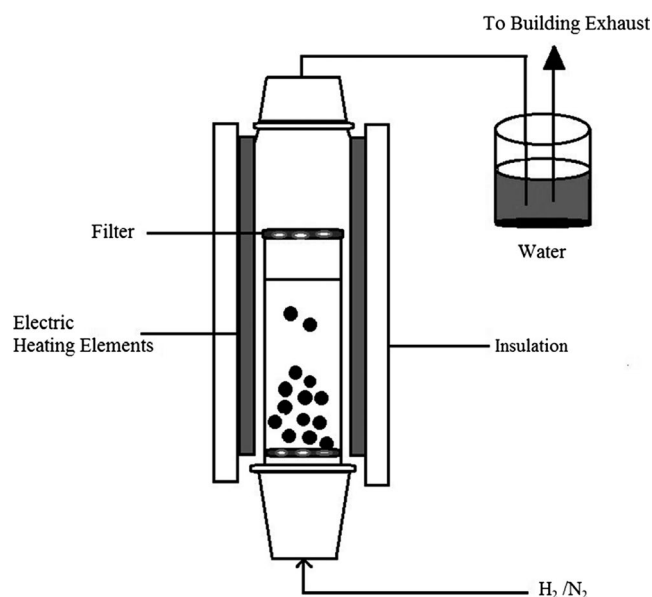
X-ray diffraction (XRD) analyses were performed on a Rigaku Rotating Anode Goniometer (Rigaku Denki., LTD., Tokyo, Japan) with  $\text{Cu K}\alpha$  radiation of 1.54 Å, a tube voltage

of 40 kV, and a tube current of 100 mA. Samples were placed in amorphous silica sample holders, and then scanned at a rate of 2°/min from 10° to 70° 2 $\theta$  in 0.02° increments. The obtained XRD patterns were analyzed by means of Jade 2010 software (Version 1.1.5 from Mater. Data, Inc.). Peak positions and relative intensities were identified in comparison with the reference powder diffraction data (JCPDS) files.

TEM studies of sample microstructures were run on a JEOL 3100R05 Double Cs Corrected TEM/STEM operated at an acceleration voltage of 300 kV with the Gatan Ultrascan 1000 CCD TV camera for high resolution imaging, and a JEOL 2100F Probe-corrected Electron Microscope at an acceleration voltage of 200 kV with an EDAX 60 mm<sup>2</sup> SDD detector (active area = 60 mm<sup>2</sup>) capable of detecting elements with  $Z > 5$ .

Thermal gravimetric analysis (TGA) and differential thermal analysis (DTA) were performed on an SDT Q600 simultaneous TGA-DTA instrument. About 20 mg of powder samples were pressed to a small pellet and loaded in an alumina pan, using an empty pan as reference. Then the samples were heated from room temperature to 1000°C at 10°C min<sup>-1</sup> in 60 mL/min of flowing air.

Fourier transform infrared spectra (FTIR) were obtained on a NICOLET 6700 using KBr discs to monitor changes in atomic bonding during chemical modification. Optical grade KBr, 400 mg (International Crystal Laboratories, Garfield, NJ), was ground using an alumina mortar and pestle, and 5 mg of sample was added and ground together. The ground samples were loaded in the FTIR sample holder, and loaded into the instrument. Then the sample chamber was purged with  $\text{N}_2$  (10-15 minutes) to remove atmospheric  $\text{CO}_2$ . Each spectrum is continuous in the range 4000-400  $\text{cm}^{-1}$  with a scan resolution of 4  $\text{cm}^{-1}$  with an average of 130 scans, using OMNIC software package.

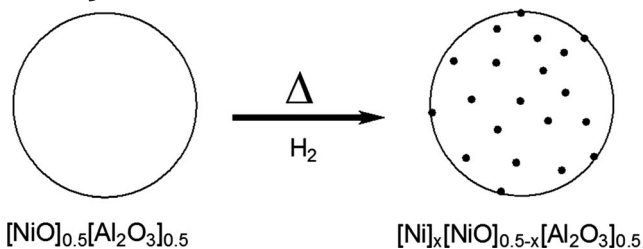


**FIGURE 1** Schematic of FBR used to reduce NPs in  $\text{H}_2/\text{N}_2$  flow at selected temperatures

## 3 | RESULTS AND DISCUSSION

The overall objective of the work reported here is to demonstrate that careful treatment of single phase but mixed-metal nanoparticles with a reducing agent can selectively reduce one component of the single phase to generate phase separation while still maintaining the nanoscale properties of the individual nanopowders. Such a process was envisioned to produce “chocolate chip” like nanocomposites with the catalytically active species decorating the partially reduced substrate, as suggested in Figure 2.

We recently demonstrated this same approach wherein treatment of nearly single phase  $(\text{TiO}_2)_{0.43}(\text{Al}_2\text{O}_3)_{0.57}$  nanopowders with  $\text{NH}_3$  reduces the  $\text{TiO}_x$  component likely by the same pathway as suggested in Figure 2 but with segregation to form more stable  $\text{TiN@Al}_2\text{O}_3$  core shell nanocomposites.<sup>59</sup> We also suspect that a similar process occurs in the



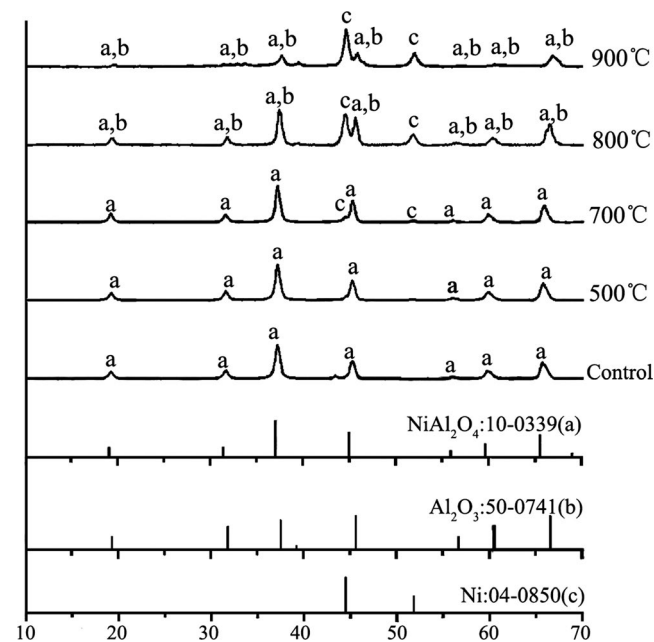
**FIGURE 2** Selective reduction of NiO species within a single phase stable spinel,  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  nanoparticle to produce a chocolate chip like Ni decorated  $[\text{Ni}]_x[\text{NiO}]_{0.5-x}[\text{Al}_2\text{O}_3]_{0.5}$  nanoparticle

transformation of  $[\text{CoO}]_{0,x}[\text{Al}_2\text{O}_3]_{1-x}$  where  $x = 0.25$  or  $0.50$  to active catalyst species in the gas phase synthesis of carbon nanotubes (CNTs) from such nanopowders under reducing conditions.<sup>58</sup>

In the current studies, we attempt to carefully define the phase separation process for the title materials to establish the basis for creating Ni nanoparticle catalysts for CNT syntheses where the spinel nanopowders are first processed into dense flexible films. The studies reported here provide an understanding of the processes that lead to catalyst particle formation in a recently published work.<sup>60</sup>

### 3.1 | Effect of reduction process on the crystal structure of as prepared nanocomposites

Figure 2 provides XRDs of as-prepared  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  NPs (control) and derived nanocomposites reduced for



**FIGURE 3** XRD patterns of as-prepared  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  NPs and nanocomposites derived there from by reduction at different temperatures for 7 h in flowing (100 mL/min) 5/95  $\text{H}_2:\text{N}_2$

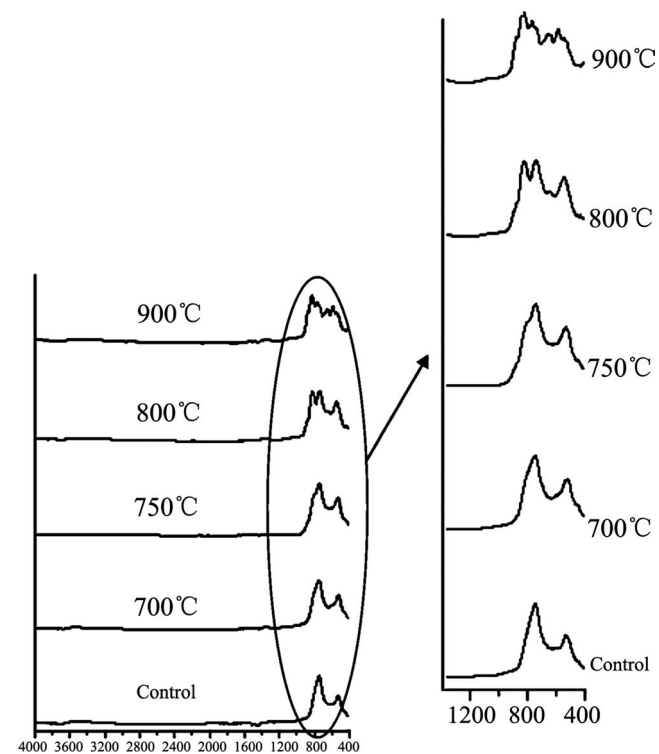
7 hours at different temperatures in flowing (100 mL/min) 5/95  $\text{H}_2:\text{N}_2$  in the course of optimizing the reduction process.

Figure 3 shows XRDs from both the as-produced  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  NPs (control) and reduced samples. The  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  spinel phase is the only phase present at reduction temperatures below  $700^\circ\text{C}$ . Above  $700^\circ\text{C}$ , diffraction peaks for cubic nickel (marked as c) appear with very weak intensities. At temperature  $800^\circ\text{C}$ , several obvious peaks for metallic nickel can be observed. Coincidentally, both nickel spinel (marked as a) and  $\text{Al}_2\text{O}_3$  (marked as b) diffraction peaks are observed. In contrast, at  $900^\circ\text{C}$  the XRD pattern shows primarily metallic Ni and  $\gamma\text{-Al}_2\text{O}_3$ . Based on this set of studies,  $800^\circ\text{C}$  was selected as the optimal temperature for producing high surface area, Ni on  $\text{Al}_2\text{O}_3$  NPs to optimize chocolate chip-like nanocomposite processing.

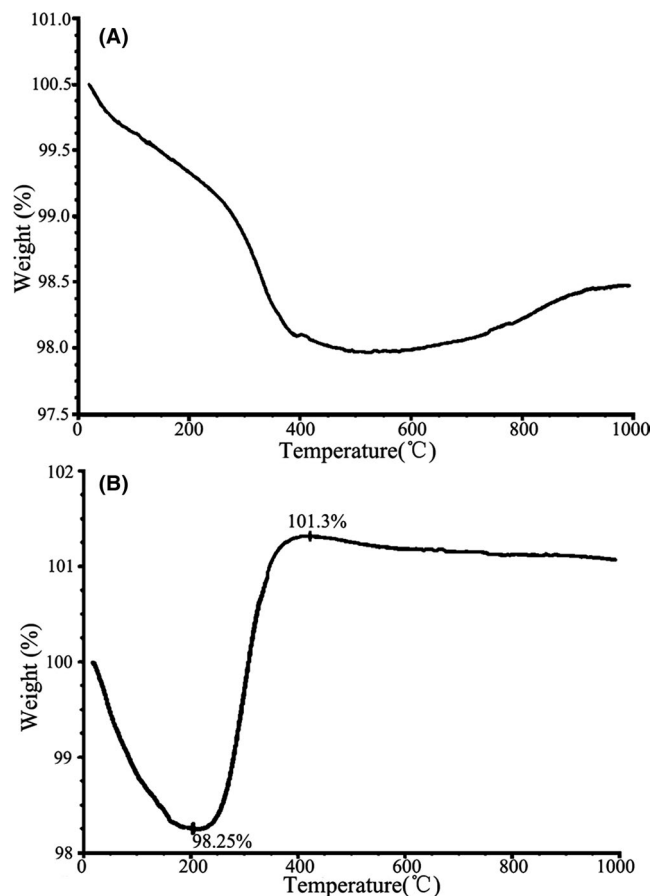
### 3.2 | Fourier transform infrared spectroscopy

To further confirm the formation of  $\text{Al}_2\text{O}_3$  in the above nanocomposites, the chemical characteristics of the different nanocomposite samples were monitored by Fourier transform infrared spectroscopy (FT-IR) as shown in Figure 4.

Figure 4 shows that a small new peak appearing around  $825\text{ cm}^{-1}$  at a reduction temperature of  $\geq 750^\circ\text{C}$ , becomes more obvious at  $800^\circ\text{C}$ . New peaks appearing near 600 and  $800\text{ cm}^{-1}$  correspond to octahedrally and tetrahedrally



**FIGURE 4** FTIR spectra from the five samples chosen from as-prepared nanocomposites by reducing LF-FSP  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  NPs at different temperatures for 7 h in flowing (100 mL/min) 5/95  $\text{H}_2:\text{N}_2$



**FIGURE 5** TGA/DTA of (A) as-produced  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  NPs and (B) after reduction at  $800^\circ\text{C}/7\text{ h}$

coordinated  $\nu\text{Al-O}$  coincident with nickel generation,<sup>45,61,62</sup> as expected from the XRD results. The new peaks become more obvious as temperatures increase to  $900^\circ\text{C}$  as metallic Ni is produced, which must coincidentally generate  $\text{Al}_2\text{O}_3$ .

### 3.3 | TGA and DTA

To obtain Ni metal contents in the above nanocomposites, TGA analyses were run of the as-produced powders and of

the  $800^\circ\text{C}$  reduced powders per Figure 5A,B. In Figure 5A, there is no obvious mass gain whereas in Figure 5B, an obvious mass gain appears between  $200^\circ$  and  $400^\circ\text{C}$ . The mass gain is directly proportional to the formation of NiO from Ni, and the Ni metal contents can be estimated to be about 11 wt %.

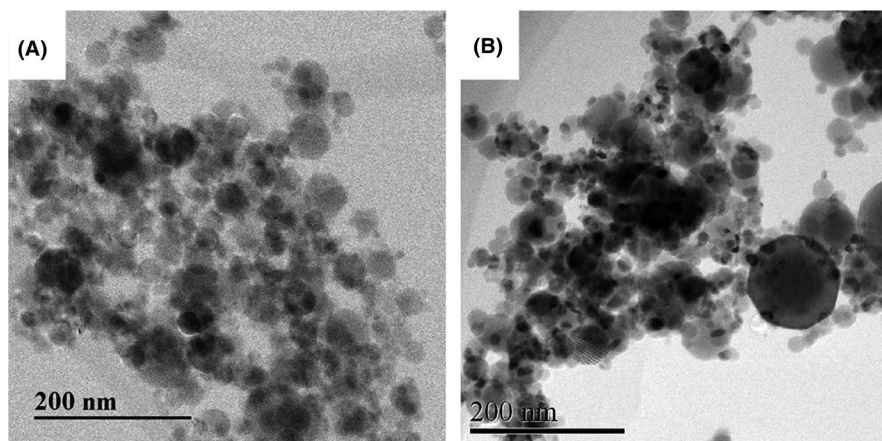
### 3.4 | Microstructures of nanocomposites

Figures 6 and 7 provide STEM bright-field (BF) and annular dark-field images and element mapping results. Figure 6 shows typical particle distributions and morphologies characteristic of  $800^\circ\text{C}$  reduced NPs. All NPs exhibit similar spherical and homogeneous morphologies, mostly smaller than 60 nm. The many dark, small spots evenly distributed on the surface of the NPs likely correspond to Ni metal particles. In Figure 7, element maps of O, Al and Ni are displayed in red, yellow and blue, respectively. As is evident both O and Al are uniformly distributed. More Ni can be observed coincident with the small dark spots distributed on the NP surfaces as anticipated.

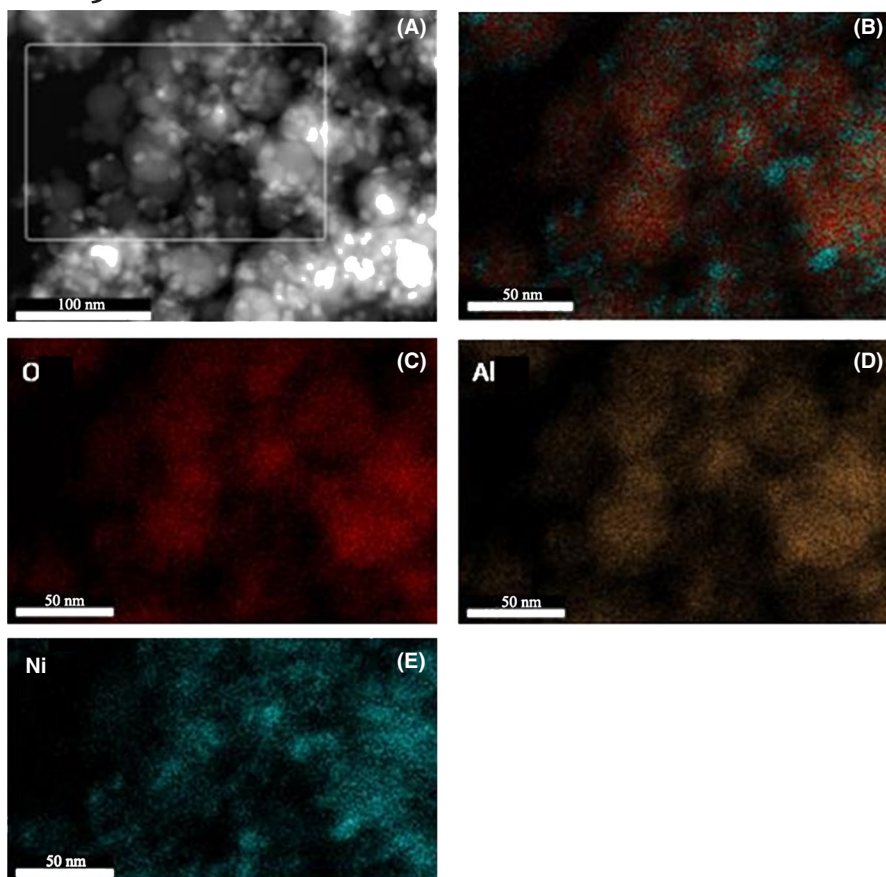
Figure 8 HRTEM provides two more complete assessments of the  $[\text{Ni}]_x[\text{NiO}]_{0.5-x}[\text{Al}_2\text{O}_3]_{0.5}$  nanocomposite morphology, confirming their chocolate chip-like microstructure. Besides, Figure 8 shows two representative nickel metal particles  $<10\text{ nm}$  in diameter, dispersed evenly on the surface of  $[\text{NiO}]_{0.5-x}[\text{Al}_2\text{O}_3]_{0.5}$  spinel NPs, confirming the formation of a chocolate chip-like nanocomposite. The same HRTEM images show  $\text{Al}_2\text{O}_3$  formed at the edge of nickel particle, consistent with the XRD and FTIR results.

## 4 | CONCLUSIONS

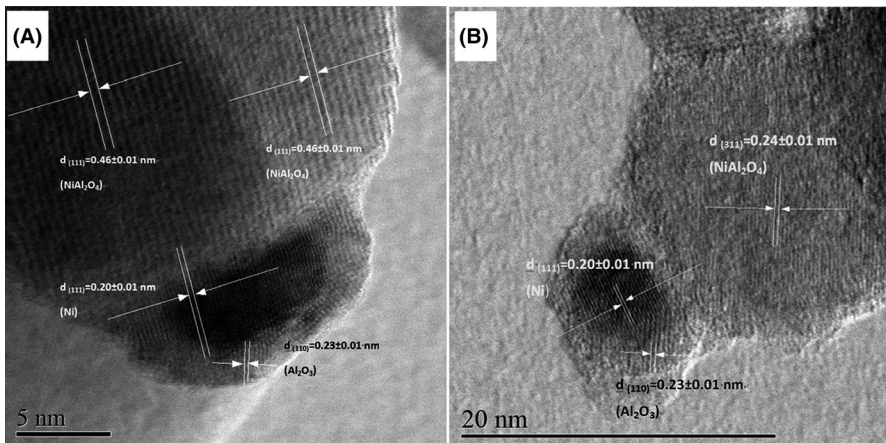
In this work, we describe a method of transforming a single phase nanopowder into a nanocomposite nanopowder without loss of nanoscale properties. This work sets the tone for the development of a series of catalysts with high surface area and presumably high activity on high surface area substrates very



**FIGURE 6** STEM BF image of nanocomposite NPs from  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  NPs before (A) and after (B) reduction at  $800^\circ\text{C}$



**FIGURE 7** Element mapping of 800°C reduced  $[\text{Ni}]_x[\text{NiO}]_{0.5-x}[\text{Al}_2\text{O}_3]_{0.5}$  nanocomposite: (A) annular dark-field image with an region for element mapping outlined; (B) color mixed element maps with Ni, O and Al showing blue, red and yellow, respectively; (C), (D) and (E) are O, Al and Ni maps [Color figure can be viewed at [wileyonlinelibrary.com](http://wileyonlinelibrary.com)]



**FIGURE 8** HRTEM images taken from two typical particles of as-prepared nanocomposites derived from the LF-FSP  $[\text{Ni}]_x[\text{NiO}]_{0.5-x}[\text{Al}_2\text{O}_3]_{0.5}$  NPs reduced at 800°C/7 h in 100 mL/min 5/95  $\text{H}_2:\text{N}_2$

difficult to generate via any other process we are aware. This work also provides the baseline science elucidating the reduction process that occurs in thin films of similar materials used as regenerable nanocomposite catalysts for carbon nanotube syntheses.<sup>60</sup> In this process, careful reduction of the nickel component in  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  spinel nanopowders in flowing 5/95  $\text{H}_2:\text{N}_2$  leads to local reduction of some portion of the NiO likely near the surface of the original nanopowders to produce a spinel nanopowder decorated with Ni metal nanoparticles. The process can be considered as an approach to make a wide variety of catalytic “chocolate chip-like” nanocomposites.

The Ni metal particle sizes appear to be typically smaller than 10 nm and evenly distributed on the surface of  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  spinel nanopowders. Coincidentally,  $\gamma\text{-Al}_2\text{O}_3$  forms at the edge of nickel particles. The limited aggregation with good stoichiometric control offers the potential to develop a number of such nanocomposite materials for catalytic applications for example. Finally, these results serve as baseline data for the catalytic reduction of  $[\text{NiO}]_{0.5}[\text{Al}_2\text{O}_3]_{0.5}$  derived thin films that can be used to catalytically generate carbon nanotubes and whose catalytic reactivity can be regenerated.<sup>60</sup> Indeed we suspect it also occurs in the gas phase

process wherein  $[\text{CoO}]_x[\text{Al}_2\text{O}_3]_{1-x}$  nanoparticles are reduced in flowing hydrogen and thereafter used to catalyze formation of carbon nanotubes as demonstrated in Figure 4 of Ref. <sup>58</sup>.

## ACKNOWLEDGMENTS

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## REFERENCES

- Kamiguchi S, Nagashima S, Chihara T. Application of solid-state early-transition metal clusters as catalysts. *Tetrahedron Lett.* 2018;59(14):1337–42.
- Suo H, Solan GA, Ma Y, Sun W. Developments in compartmentalized bimetallic transition metal ethylene polymerization catalysts. *Coord Chem Rev.* 2018;372:101–16.
- Takenaka S, Kaji R, Sugiyama K, Ida R. Preparation of composite catalysts composed of Pt nanoparticles and metal oxide nanosheets: preferential formation of Pt/metal oxide interfaces. *Appl Catal, A.* 2018;566:52–9.
- Hita I, Deuss P, Bonura G, Frusteri F, Heeres H. Biobased chemicals from the catalytic depolymerization of Kraft lignin using supported noble metal-based catalysts. *Fuel Process Technol.* 2018;179:143–53.
- Almutairi S, Kozhevnikova E, Kozhevnikov I. Ketonisation of acetic acid on metal oxides: Catalyst activity, stability and mechanistic insights. *Appl Catal, A.* 2018;565:135–45.
- Schmal M, Toniolo FS, Kozonoe CE. Perspective of catalysts for (Tri) reforming of natural gas and flue gas rich in  $\text{CO}_2$ . *Appl Catal, A.* 2018;568:23–42.
- Huang H, Lu H, Zhan Y, Liu G, Feng Q, Huang H, et al. VUV photo-oxidation of gaseous benzene combined with ozone-assisted catalytic oxidation: Effect on transition metal catalyst. *Appl Surf Sci.* 2017;391:662–7.
- Min JE, Lee YJ, Park HG, Zhang C, Jun KW. Carbon dioxide reforming of methane on Ni-MgO- $\text{Al}_2\text{O}_3$  catalysts prepared by sol-gel method: effects of Mg/Al ratios. *J Ind Eng Chem.* 2015;26:375–83.
- Shin D, An X, Choun M, Lee J. Effect of transition metal induced pore structure on oxygen reduction reaction of electrospun fibrous carbon. *Catal Today.* 2016;260:82–8.
- Salam MA, Abdullah B. Catalysis mechanism of Pd-promoted  $\gamma$ -alumina in the thermal decomposition of methane to hydrogen: a density functional theory study. *Mater Chem Phys.* 2017;188:18–23.
- Wang F, Xie Z, Liang J, Fang B, Piao Y, Hao M, et al. Tourmaline-modified  $\text{FeMnTiO}_x$  catalysts for improved low-temperature  $\text{NH}_3$ -SCR performance. *Environ Sci Technol.* 2019;00:1–8. <https://doi.org/10.1021/acs.est.9b02620>
- Keum C, Kim MC, Lee SY. Effects of transition metal ions on the catalytic activity of carbonic anhydrase mimics. *J Mol Catal A: Chem.* 2015;408:69–74.
- Manukyan KV, Cross AJ, Yeghishyan AV, Rouvimov S, Miller JJ, Mukasyan AS, et al. Highly stable Ni- $\text{Al}_2\text{O}_3$  catalyst prepared from a Ni-Al layered double hydroxide for ethanol decomposition toward hydrogen. *Appl Catal, A.* 2015;508:37–44.
- Salazar A, Chave T, Ayril A, Nikitenko SI, Hulea V, Kooyman PJ, et al. Engineering of silica-supported platinum catalysts with hierarchical porosity combining latex synthesis, sonochemistry and sol-gel process—I. Material preparation. *Micropor Mesopor Mat.* 2016;234:207–14.
- Jiménez-González C, Boukha Z, Rivas BD, González-Velasco JR, Gutiérrez-Ortiz JI, López-Fonseca R. Behavior of coprecipitated  $\text{NiAl}_2\text{O}_4/\text{Al}_2\text{O}_3$  catalysts for low-temperature methane steam reforming. *Energy Fuels.* 2014;28:7109–21.
- Banerjee AM, Pai MR, Tewari R, Raje N, Tripathi AK, Bharadwaj SR, et al. A comprehensive study on Pt/ $\text{Al}_2\text{O}_3$  granular catalyst used for sulfuric acid decomposition step in sulfur-iodine thermochemical cycle: Changes in catalyst structure, morphology and metal-support interaction. *Appl Catal, B.* 2015;162:327–37.
- Zhou L, Li L, Wei N, Li J, Takane K, Basset JM. Effect of  $\text{NiAl}_2\text{O}_4$  formation on Ni/ $\text{Al}_2\text{O}_3$  stability during dry reforming of methane. *ChemCatChem.* 2015;7(16):2406–2406.
- Yuan P, Cui C, Han W, Bao X. The preparation of Mo/ $\gamma$ - $\text{Al}_2\text{O}_3$  catalysts with controllable size and morphology via adjusting the metal-support interaction and their hydrodesulfurization performance. *Appl Catal, A.* 2016;524:115–25.
- Tao M, Meng X, Lv Y, Bian Z, Xin Z. Effect of impregnation solvent on Ni dispersion and catalytic properties of Ni/SBA-15 for CO methanation reaction. *Fuel.* 2016;165(4):289–97.
- Wen X, Li R, Yang Y, Chen J, Zhang F. An egg-shell type Ni/ $\text{Al}_2\text{O}_3$  catalyst derived from layered double hydroxides precursor for selective hydrogenation of pyrolysis gasoline. *Appl Catal, A.* 2013;468:204–15.
- Li B, Qian X, Wang X. Oxidative  $\text{CO}_2$  reforming of methane over stable and active nickel-based catalysts modified with organic agents. *Int J Hydrogen Energy.* 2015;40(25):8081–92.
- Danilova MM, Fedorova ZA, Zaikovskii VI, Porsin AV, Kirillov VA, Krieger TA. Porous nickel-based catalysts for combined steam and carbon dioxide reforming of methane. *Appl Catal, B.* 2014;147(7):858–63.
- Takahashi S, Kan A, Ogawa H. Microwave dielectric properties and crystal structures of spinel-structured  $\text{MgAl}_2\text{O}_4$  ceramics synthesized by a molten-salt method. *J Eur Ceram Soc.* 2017;37(3):1001–6.
- Li D, Lu M, Cai Y, Cao Y, Zhan Y, Jiang L. Synthesis of high surface area  $\text{MgAl}_2\text{O}_4$  spinel as catalyst support via layered double hydroxides-containing precursor. *Appl Clay Sci.* 2016;132:243–50.
- Gupta SK, Pathak N, Ghosh PS, Kadam RM. On the photophysics and speciation of actinide ion in  $\text{MgAl}_2\text{O}_4$  spinel using photoluminescence spectroscopy and first principle calculation: a case study with uranium. *J Alloys Compd.* 2017;695:337–43.
- Samkaria R, Sharma V. Effect of rare earth yttrium substitution on the structural, dielectric and electrical properties of nanosized nickel aluminate. *Mater Sci Eng, B.* 2013;178(20):1410–5.

27. Santillan-Jimenez E, Loe R, Garrett M, Morgan T, Crocker M. Effect of Cu promotion on cracking and methanation during the Ni-catalyzed deoxygenation of waste lipids and hemp seed oil to fuel-like hydrocarbons. *Catal Today*. 2018;302:261–71.
28. He L, Hui H, Li S, Lin W. Production of light aromatic hydrocarbons by catalytic cracking of coal pyrolysis vapors over natural iron ores. *Fuel*. 2018;216:227–32.
29. Thattarathody R, Sheintuch M. Kinetics and dynamics of methanol steam reforming on CuO/ZnO/alumina catalyst. *Appl Catal, A*. 2017;540:47–56.
30. Bagherzadeh SB, Haghghi M. Plasma-enhanced comparative hydrothermal and coprecipitation preparation of CuO/ZnO/Al<sub>2</sub>O<sub>3</sub> nanocatalyst used in hydrogen production via methanol steam reforming. *Energy Convers Manage*. 2017;142:452–65.
31. Correa A, Cascella M, Scotti N, Zaccheria F, Ravasio N, Psaro R. Mechanistic insights into formic acid dehydrogenation promoted by Cu-amino based systems. *Inorg Chim Acta*. 2018;470:290–4.
32. Kalenchuk AN, Bogdan VI, Dunaev SF, Kustov LM, Dunaev SF, Kustov LM. Dehydrogenation of polycyclic naphthenes on a Pt/C catalyst for hydrogen storage in liquid organic hydrogen carriers. *Fuel Process Technol*. 2018;169:94–100.
33. Karaman BP, Cakiryilmaz N, Arbag H, Oktar N, Dogu G, Dogu T. Performance comparison of mesoporous alumina supported Cu & Ni based catalysts in acetic acid reforming. *Int J Hydrogen Energy*. 2017;42(42):26257–69.
34. Papageridis KN, Siakavelas G, Charisiou ND, Avraam DG, Tzounis L, Kousi K, et al. Comparative study of Ni Co, Cu supported on  $\gamma$ -alumina catalysts for hydrogen production via the glycerol steam reforming reaction. *Fuel Process Technol*. 2016;152:156–75.
35. Kim D, Jeon J, Lee W, Lee J, Ha KS. Effective suppression of deactivation by utilizing Ni-doped ordered mesoporous alumina-supported catalysts for the production of hydrogen and CO gas mixture from methane. *Int J Hydrogen Energy*. 2017;42(39):24744–56.
36. Braidly N, Bastien S, Blanchard J, Fauteux-Lefebvre C, Achouri IE, Abatzoglou N. Activation mechanism and microstructural evolution of a YSZ/Ni-alumina catalyst for dry reforming of methane. *Catal Today*. 2017;291:99–105.
37. Jiménez-González C, Boukha Z, Rivas BD, González-Velasco JR, Gutiérrez-Ortiz JI, López-Fonseca R. Behaviour of nickel–alumina spinel (NiAl<sub>2</sub>O<sub>4</sub>) catalysts for isooctane steam reforming. *Int J Hydrogen Energy*. 2015;40(15):5281–8.
38. Shamskar FR, Meshkani F, Rezaei M. Ultrasound assisted co-precipitation synthesis and catalytic performance of mesoporous nanocrystalline NiO–Al<sub>2</sub>O<sub>3</sub> powders. *Ultrason Sonochem*. 2017;34:436–47.
39. Kumar JP, Prasad GK, Allen JA, Ramacharyulu P, Kadirvelu K, Singh B. Synthesis of mesoporous metal aluminate nanoparticles and studies on the decontamination of sulfur mustard. *J Alloys Compd*. 2016;662:44–53.
40. Neto A, Oliveira AC, Filho JM, Amadeo N, Dieuzeide ML, de Sousa FF, et al. Characterizations of nanostructured nickel aluminates as catalysts for conversion of glycerol: Influence of the preparation methods. *Adv Powder Technol*. 2017;28(1):131–8.
41. Achouri IE, Abatzoglou N, Fauteux-Lefebvre C, Braidly N. Diesel steam reforming: Comparison of two nickel aluminate catalysts prepared by wet-impregnation and co-precipitation. *Catal Today*. 2013;207:13–20.
42. Nieva MA, Villaverde MM, Monzón A, Garetto TF, Marchi AJ. Steam-methane reforming at low temperature on nickel-based catalysts. *Chem Eng J*. 2014;235:158–66.
43. Yi JH, Kim JH, Koo HY, You NK, Kang YC, Lee JH. Nanosized LiMn<sub>2</sub>O<sub>4</sub> powders prepared by flame spray pyrolysis from aqueous solution. *J Power Sources*. 2011;196(5):2858–62.
44. Demirci S, Öztürk B, Yildirim S, Bakal F, Erol M, Sancakoğlu O, et al. Synthesis and comparison of the photocatalytic activities of flame spray pyrolysis and sol–gel derived magnesium oxide nanoscale particles. *Mater Sci Semicond Process*. 2015;34:154–61.
45. Kim JH, Hong YJ, Park BK, Kang YC. Nano-sized LiNi<sub>0.5</sub>Mn<sub>1.5</sub>O<sub>4</sub> cathode powders with good electrochemical properties prepared by high temperature flame spray pyrolysis. *J Ind Eng Chem*. 2013;19(4):1204–8.
46. Kruijs FE, Fissan H, Peled A. Synthesis of nanoparticles in the gas phase for electronic, optical and magnetic applications—a review. *J Aerosol Sci*. 1998;29(5–6):511–35.
47. Schimmoeller B, Schulz H, Ritter A, Reitzmann A, Kraushaarzarnetzki B, Baiker A, et al. Structure of flame-made vanadia/titania and catalytic behavior in the partial oxidation of oxylene. *J Catal*. 2008;256(1):74–83.
48. Wagner N, Svensson AM, Vullum-Bruer F. Liquid-feed flame spray pyrolysis as alternative synthesis for electrochemically active nano-sized Li<sub>2</sub>MnSiO<sub>4</sub>. *Transl Mater Res*. 2016;3(2):025001.
49. Suffner J, Wang D, Kübel C, Hahn H. Metastable phase formation during flame spray pyrolysis of ZrO(YO)–AlO nanoparticles. *Scr Mater*. 2011;64(8):781–4.
50. Hinklin T, Toury B, Gervais C, Babonneau F, Gislason Jj, Morton R, et al. Liquid-feed flame spray pyrolysis of metalloorganic and inorganic alumina sources in the production of nanoalumina powders. *Chem Mater*. 2004;16(1):21–30.
51. Laine RM, Bickmore CR, Treadwell DR, Waldner KF. Ultrafine metal oxide powders by flame spray pyrolysis. U.S. Patent 5958361. 1999 Sep. 28.
52. Baranwal R, Villar M, Garcia R, Laine R. Synthesis, characterization, and sintering behavior of nano-mullite powder and powder compacts. *J Am Ceram Soc*. 2001;84(5):951–61.
53. Jose AA, Julien M, Patrick S, Haiping S, Xiaoqing QP, Richard ML. Liquid-feed flame spray pyrolysis as a method of producing mixed-metal oxide nanopowders of potential interest as catalytic materials. nanopowders along the NiO–Al<sub>2</sub>O<sub>3</sub> tie line including (NiO)<sub>0.22</sub>(Al<sub>2</sub>O<sub>3</sub>)<sub>0.78</sub>, a new inverse spinel composition. *Chem. Mater*. 2006;18(9):731–9.
54. Taylor NJ, Stangeland-Molo S, Laine RM. Bottom-up vs reactive sintering of Al<sub>2</sub>O<sub>3</sub>-YAG-YSZ composites via one or three-phase nanoparticles (NPs). Bottom-up processing wins this time. *J Am Ceram Soc*. 2017;100(6):2429–38.
55. Li B, Williams G, Rand SC, Hinklin T, Laine RM. Continuous-wave ultraviolet laser action in strongly scattering Nd-doped alumina. *Opt Lett*. 2002;27(6):394–6.
56. Williams GR, Bayram SB, Rand SC, Hinklin T, Laine RM. Laser action in strongly scattering rare-earth-metal-doped dielectric nanophosphors. *Phys Rev A*. 2001;65(1):337–9.
57. Weidenhof B, Reiser M, Stöwe K, Maier Wf, Kim M, Azurdia J, et al. High-throughput screening of nanoparticle catalysts made by flame spray pyrolysis as hydrocarbon/NO oxidation catalysts. *J Am Chem Soc*. 2009;131(26):9207–19.
58. Shirae H, Hasegawa K, Sugime H, Yi E, Laine RM, Noda S. Catalyst nucleation and carbon nanotube growth from flame-synthesized Co–Al–O nanopowders at ten-second time scale. *Carbon*. 2017;114:31–8.
59. You F, Sun K, Yi E, Nakatani E, Umehara N, Laine RM. Chemical modification at and within nanopowders: Synthesis of core-shell



- Al<sub>2</sub>O<sub>3</sub>@TiON nanopowders via nitriding nano-(TiO<sub>2</sub>)<sub>0.43</sub> (Al<sub>2</sub>O<sub>3</sub>)<sub>0.57</sub> powders in NH<sub>3</sub>. *J Am Ceram Soc.* 2018;101(4):1441–52.
60. Liang B, Yi E, Sato T, Noda S, Jia D, Zhou Y, et al. Flame synthesized [NiO]<sub>0.25</sub>[Al<sub>2</sub>O<sub>3</sub>]<sub>0.75</sub> and [NiO]<sub>0.50</sub>[Al<sub>2</sub>O<sub>3</sub>]<sub>0.50</sub> nanopowders (NPs) provide thin, dense, flexible NiAl<sub>2</sub>O<sub>4</sub>-Al<sub>2</sub>O<sub>3</sub> and Ni-Al<sub>2</sub>O<sub>3</sub> nanocomposite catalytic films. Regeneration of a heterogeneous catalyst by oxidative re-adsorption into a heterogeneous substrate is demonstrated for carbon nanotube syntheses. Submitted for publication.
61. Taylor NJ, Pottebaum AJ, Uz V, Laine RM. The bottom up approach is not always the best processing method: dense α-Al<sub>2</sub>O<sub>3</sub>/NiAl<sub>2</sub>O<sub>4</sub> composites. *Adv Funct Mater.* 2014;24(22):3392–8.
62. Gullapelli S, Scurrill MS, Valluri DK. Photocatalytic H<sub>2</sub> production from glycerol–water mixtures over Ni/γ-Al<sub>2</sub>O<sub>3</sub> and TiO<sub>2</sub> composite systems. *Int J Hydrogen Energy.* 2017;42(22):15031–43.

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