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**Turning Trash into Treasure: MXene with Intrinsic LiF Solid Electrolyte Interfaces Performs Better and Better during Battery Cycling**

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### Abstract

Commercialization of lithium ion batteries has accelerated dramatically over the last few decades. Single-layered MXene ( $s-Ti_3C_2$ ) is effectively prepared by etching  $Ti_3AlC_2$  via simple treatment with HCl and LiF, producing inevitably sediments always discarded after etching. This study explores the effect of LiF doping of multi-layered  $Ti_3C_2$  to form  $m-Ti_3C_2/LiF$  consisting essentially of the sediments. Simple half-cells assembled with  $m-Ti_3C_2/LiF$  sediments suggest that LiF suppresses electrode volume expansion and surface cracking during cycling promoting  $Li^+$  intercalation/deintercalation. The data also suggest that LiF promotes formation of stable artificial solid electrolyte interfaces (SEIs) to prevent electrolyte and electrode degradation. The capacity of  $m-Ti_3C_2/LiF$  sediments derived cells maintains 136 mAh  $g^{-1}$  after 1500 cycles at 300 mA  $g^{-1}$  while  $s-Ti_3C_2$  from supernatants physically mixed with 20 wt. % LiF shows a capacity of 335 mAh  $g^{-1}$  (100<sup>th</sup> cycle) at 100 mA  $g^{-1}$  with an initial

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coulombic efficiency of 83 %. Half-cell anodes made of  $\text{Ti}_3\text{C}_2$  etched by HF, commercial  $\text{TiO}_2$  and Sn powder mixed physically with 20 wt. % LiF exhibit improved performance with cycling. These results indicate that the always discarded sediments can be directly used in LIBs and simple doping with LiF obviously improves the electrochemical performance of materials.

## 1. Introduction

Rechargeable lithium ion batteries (LIBs) are sought as a means to meet society's ever-increasing energy demands. Motivation comes from the fact that LIBs offer potential environment as eco-friendly, sustainable and highly effective energy sources.<sup>[1-4]</sup> Thus, great efforts are being made to enhance energy densities and power output of LIBs.<sup>[5]</sup> In particular, significant focus is on greatly improving current anode materials. Mainstream graphite anodes LIBs (theoretical capacity of  $372 \text{ mAh g}^{-1+}$ ) offer insufficient rate capabilities and suffer from uneven lithium plating.<sup>[6, 7]</sup>

The discovery, by Novoselov and Geim et al. of a method of preparing two-dimensional (2-D) materials (graphene) has attracted worldwide attention.<sup>[8]</sup> Graphene-like materials can offer excellent optical, electric and magnetic properties, which make them attractive for applications in a wide variety of energy storage and conversion devices.<sup>[9-12]</sup> These materials include hexagonal boron nitride (h-BN),<sup>[13]</sup> transition metal disulfides (TMDs),<sup>[12]</sup> metal oxides and bilayer hydroxides.<sup>[14]</sup>

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Recent reports on 2-D transition metal carbides and carbonitrides, MXenes,<sup>[15, 16]</sup> have prompted efforts to consider them for battery applications.<sup>[17]</sup> MXene materials are prepared mainly by selectively etching the A layers from the three dimensional (3-D)  $M_{n+1}AlX_n$  ( $n= 1, 2, 3$ ) parent phase, where “M” represents a transition metal, “A” is a group III or IV-A element and X is carbon and/or nitrogen. The exfoliation process was initially conducted using hydrofluoric acid (HF), producing multi-layered  $M_{n+1}X_n$  ( $m$ - $M_{n+1}X_n$ ) with surface functional OH, F, and O groups. A more benign approach uses concentrated hydrochloric acid (HCl) and lithium fluoride (LiF) mixtures as the etching medium resulting in colloidal supernatant. The colloidal supernatant is composed predominantly of single-layered  $M_{n+1}X_n$  ( $s$ - $M_{n+1}X_n$ ) coincident with  $Li^+$  intercalation,<sup>[18]</sup> while the sediments contain primarily  $m$ - $M_{n+1}X_n$  and intercalated LiF.

MXenes have now been explored extensively for electrochemical energy storage,<sup>[19-21]</sup> in electronic devices,<sup>[22, 23]</sup> as hydrogen storage materials,<sup>[24]</sup> and as separation membranes.<sup>[25]</sup>

$Ti_3C_2$ , a typical MXene, has drawn considerable attention for use in LIBs. Tang et al. described DFT calculations indicating that pure  $Ti_3C_2$  should offer a theoretical specific capacity of 320 mAh  $g^{-1}$  as anodes for LIBs with the capacity decreasing to 130 mAh  $g^{-1}$  and 67 mAh  $g^{-1}$  when  $Ti_3C_2$  is superficially functionalized with F ( $Ti_3C_2F_2$ ) and OH [ $Ti_3C_2(OH)_2$ ] respectively.<sup>[26]</sup> These surface functionalized  $Ti_3C_2$  materials were reported to exhibit a capacity of 124 mAh  $g^{-1}$  at 320 mA  $g^{-1}$  after 100 cycles due to  $Li^+$  intercalation via a conversion reaction.<sup>[27]</sup>

Numerous  $Ti_3C_2$  composites have been synthesized targeting improved electrochemical performance,<sup>[28]</sup> including  $Ti_3C_2@rGO$ ,<sup>[20]</sup>  $Ti_3C_2@CNTs$ ,<sup>[29]</sup>  $Ti_3C_2@TiO_2$ ,<sup>[30]</sup>  $Ti_3C_2@SnO_2$ ,<sup>[31]</sup>

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$\text{Ti}_3\text{C}_2@\text{Si}$ .<sup>[32]</sup>  $\text{Ti}_3\text{C}_2$  offers hydrophilic surfaces, electronic conductivity, low operating voltages 0.2-0.6 V versus  $\text{Li}^+/\text{Li}$ , low diffusion barriers (due to surface functional groups) and stable layered structures (due to Ti-C bonds) with exceptional mechanical properties, which are important to  $\text{Li}^+$  intercalation.<sup>[31]</sup> Therefore,  $\text{Ti}_3\text{C}_2$  seems to be an ideal matrix template for LIB anode composites.<sup>[33]</sup>

Single-layered  $\text{Ti}_3\text{C}_2$  (*s*- $\text{Ti}_3\text{C}_2$ ) is easily obtained by first etching Al from  $\text{Ti}_3\text{AlC}_2$  and then delaminating the multilayered  $\text{Ti}_3\text{C}_2$  (*m*- $\text{Ti}_3\text{C}_2$ ) using HCl and LiF. This stepwise procedure generates mixtures of undelaminated *m*- $\text{Ti}_3\text{C}_2$  containing up to 90% of the original LiF used.<sup>[34]</sup> The *m*- $\text{Ti}_3\text{C}_2/\text{LiF}$  sediments are normally ignored or disposed, which greatly increases synthesis cost and hinders applications in LIBs. Note that LiF is the main inorganic component in solid electrolyte interfaces (SEIs) that form in commercial LIBs, offering a wide electrochemical stability window with negligible solubility in most electrolytes solvents as well as a relatively low energy barrier for  $\text{Li}^+$  diffusion.<sup>[35, 36]</sup>

Peng et al. developed a transplantable LiF-rich layer (TLL) to improve the cycling stability of Li metal anodes where  $\text{Li}^+$  can diffuse through this artificial layer and deposit on the Cu or Li substrate surfaces.<sup>[37]</sup> Sun et al. developed an extremely simple cell formation process to simultaneously form LiF-rich protective-films on the surfaces of both CNT-cathodes and Li metal anodes.<sup>[38]</sup> Shen et al. successfully prepared GF (graphite fluoride)-LiF-Li composites that bond with metallic lithium and are stable on contact with a carbonate electrolyte.<sup>[39]</sup> Zhu et al. showed that the lithium storage performance of  $\text{MoS}_2$  could be improved by facilitating the generation of a robust LiF-rich SEI by adding fluoroethylene carbonate (FEC) to prevent

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continuous electrolyte decomposition.<sup>[40]</sup> On this basis, the resulting sediments produced here were chosen as a starting point to develop anodes for LIBs with well-defined architecture.

The objective of the current work is to show how LiF influences the electrochemical performance of *m*-Ti<sub>3</sub>C<sub>2</sub>/LiF sediment anodes for LIBs. The source of these materials from sediments is simply the “debris” recovered from the etching process without additional additives and displays some abnormal (advantageous) electrochemical properties. The rationally fabricated cells exhibit gradually increasing capacities after initial capacity fading, in which they maintain 198 mAh g<sup>-1</sup> (600<sup>th</sup> cycle) at 30 mA g<sup>-1</sup> and 136 mAh g<sup>-1</sup> (1500<sup>th</sup> cycle) at 300 mA g<sup>-1</sup> while *s*-Ti<sub>3</sub>C<sub>2</sub> from supernatants physically mixed with 20 wt. % LiF shows a reversible capacity of 335 mAh g<sup>-1</sup> (100<sup>th</sup> cycle) at 100 mA g<sup>-1</sup>, which is comparable to previous reports of MXene anodes for LIBs (**Table S1**, supporting information). Additionally, intrinsic LiF serves as an artificial SEI and Li<sup>+</sup> diffusion shuttle, appearing to play a significant role in restraining the expansion and cracking of electrodes as well as improving the electrochemical performance.

## 2. Results and discussion

**Figure 1** provides a general overview of the processing steps (detailed in Experimental Section, supporting information) that lead to formation of *m*-Ti<sub>3</sub>C<sub>2</sub>/LiF(S<sub>1</sub>) consisting of sediments and *s*-Ti<sub>3</sub>C<sub>2</sub> consisting of supernatants via HCl+LiF etching of Ti<sub>3</sub>AlC<sub>2</sub>. The *m*-Ti<sub>3</sub>C<sub>2</sub>/LiF(S<sub>1</sub>) is easily separated from *s*-Ti<sub>3</sub>C<sub>2</sub> supernatant by high speed centrifugation.

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**Figure S1** (supporting information) presents XRD analyses of some samples. The precursor XRD pattern,  $\text{Ti}_3\text{AlC}_2$  powder, presents characteristic peaks labeled as  $\blacklozenge$ . The peaks marked as  $\star$  of  $\text{Ti}_3\text{C}_2$  etched by HF suggest some loss of crystallinity with structural distortions compared with  $\text{Ti}_3\text{AlC}_2$ . Also, the characteristic (002) and (004) planes broaden and shift to lower angles  $2\theta$  arising from increases in d- and layer- spacing. Notably, the intensity of the peak at  $\approx 39^\circ 2\theta$ , corresponding to the (104) plane of the  $\text{Ti}_3\text{AlC}_2$ , weakens significantly, suggesting successful removal of Al layers from  $\text{Ti}_3\text{AlC}_2$  and formation of  $\text{Ti}_3\text{C}_2$ .<sup>[41]</sup>

In addition,  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  diffraction peaks match closely those of  $\text{Ti}_3\text{C}_2$  including (002), (103), (105) and (112) planes (marked as  $\star$ ). The LiF peak pattern, especially for (111), (200) and (220) planes, is also clearly present (marked as  $\blacktriangle$ ). These peaks are un-shifted vs. crystalline LiF, indicating its presence after etching. Moreover, (002) peak of  $\text{Ti}_3\text{AlC}_2$  appears in this pattern, indicating that not all the  $\text{Ti}_3\text{AlC}_2$ -phase converts to  $m\text{-Ti}_3\text{C}_2$ , while a small amount of  $\text{Ti}_3\text{AlC}_2$  exists in the sediments further evidenced by EDX and XPS. Besides, the presence of a  $\approx 39^\circ 2\theta$  peak (**Figure S2**, supporting information) shows that etching using  $\text{MgF}_2+\text{HCl}$  offers end-products of  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$ , demonstrating relatively low etching efficiency.

The morphologies of  $\text{Ti}_3\text{AlC}_2$ , LiF,  $\text{Ti}_3\text{C}_2$ ,  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  and  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$  were characterized by SEM and TEM. As shown in **Figure 2a**,  $\text{Ti}_3\text{AlC}_2$  presents irregular, 3-D blocks. **Figure 2b** exhibits typical LiF cube morphology. **Figure S3** and **Table S2** (supporting information) show typical book-like morphology and elemental mapping results of  $\text{Ti}_3\text{C}_2$ , which are typical etching results by HF. **Figure 2c** shows that the remaining LiF particles are

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mixed with the  $m\text{-Ti}_3\text{C}_2$  particles after HCl+LiF etching. To verify the success of the etching procedure when HCl and LiF were used, EDX analyses of  $m\text{-Ti}_3\text{C}_2$  selected from local areas in **Figure 2g** of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  are presented in **Figure 2h** and **Table S3** (supporting information). These results demonstrate that C, O, F, Al and Ti are homogeneously distributed. Mapping for Al shows a minimal amounts of 1.58 wt. %, mainly ascribed to the un-reacted  $\text{Ti}_3\text{AlC}_2$ .

During the reaction process, excess dissolved LiF apparently penetrates the layered structure and crystallizes within the resulting samples and remains even after etchant treated samples are rinsed more than a dozen times. Coincident with etching and deposition of LiF nanoparticles the smooth surface gradually erodes (**Figure 2d**). In contrast, **Figure S4** (supporting information) shows that the formed  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$  retain their book-like morphology with rough surfaces. Elemental mapping results (**Table S4**, supporting information) indicating that Al is not fully etched by HCl+ $\text{MgF}_2$ .

TEM images of  $\text{Ti}_3\text{C}_2$  etched by HF and HCl+LiF reveal separated layers. The results are in good agreement with the above SEM results. The formed edges are similar to the graphitic layers reported previously.<sup>[42]</sup> The cross-sectional HRTEM images in **Figure 2e-f** show that the layer spacing of  $\text{Ti}_3\text{C}_2$  etched by HCl+LiF is 1.14 nm, a little larger than that etched by HF alone (0.98 nm). The inset in **Figure 2e** does not show similar hexagonal packing behavior, see inset in **Figure 2f**, most easily interpreted as being caused by the presence of crystalline LiF and  $\text{Ti}_3\text{AlC}_2$ . The distinct interlayer pores of etched  $\text{Ti}_3\text{C}_2$  provide sites for  $\text{Li}^+$  interaction.<sup>[43]</sup>

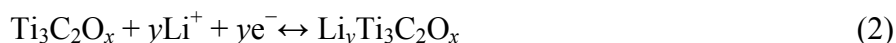


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XPS was used to confirm the chemical composition, bonding, and oxidation states in the  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$ . The low-resolution survey spectrum (**Figure 3a**) shows that typical elemental signatures for  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  primarily consist of Ti, O, C, F and Li. The LiF content is calculated to be 36.8 wt. % (**Table S5**, supporting information). As presented in **Figure 3b**, XPS peak fitting indicates that the Ti 2p spectrum of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  can be resolved into four sets of  $2p_{3/2}$  - $2p_{1/2}$  spin-orbit doublets with a fixed area ratio of 2:1 and doublet separation of 5.7 eV. The Ti  $2p_{3/2}$  peaks centered at 454.5, 455.8, 456.8 and 458.5 eV correspond to Ti-C,  $\text{Ti}^{2+}$ ,  $\text{Ti}^{3+}$  and Ti-O, respectively.<sup>[44-46]</sup> A small amount of  $\text{TiO}_2$  forms from reaction between  $\text{Ti}_3\text{C}_2$  and the OH caused by heat generated during HCl+LiF treatment as reported previously.<sup>[47]</sup> The C 1s binding energies presented in **Figure 3c** at 289.7, 287.1, 285.1 and 282.8 eV correspond to O-C=O and C-F, C-O, C-C and Ti-C.<sup>[48]</sup> In addition, the O 1s spectrum for  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  presents peaks at 530.6, 532.4 and 534.6 eV (**Figure 3d**), matching Ti-O in  $\text{TiO}_2$ , C-Ti-O<sub>x</sub> and C-Ti-(OH)<sub>x</sub> respectively.<sup>[31]</sup> Compared with those for  $\text{Ti}_3\text{C}_2$  etched by HF alone (**Figure S5**, supporting information), there is a slight increase in the intensity of the  $\text{Ti}^{3+}$ ,  $\text{Ti}^{2+}$ , C-C, C-Ti peaks accompanied by a decrease in the intensity of Ti-O, C-F, C-O and C-Ti-(OH)<sub>x</sub> peaks. (**Table S6-7**, supporting information) The results indicate somewhat greater oxidation of Ti and formation of  $\text{TiO}_2$  during the HCl+LiF etching process.

LIB anodes prepared from the  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  were assembled, see experimental section. CV curves in voltage range of 0.01-3.00 V at a sweep rate of 0.1  $\text{mV s}^{-1}$  are shown in **Figure 4a** for the first three cycles. During the initial lithiation, irreversible peaks are observed at 0.76, 1.43 and 1.64 V, close to those of  $\text{Ti}_3\text{C}_2$  (0.8 and 1.56 V) presented in **Figure S6** (supporting

information). However, they are absent in subsequent cycles, ascribed to formation of a SEI and trapping of  $\text{Li}^+$  between  $\text{Ti}_3\text{C}_2$  flakes in the electrode.<sup>[49]</sup> In the first delithiation step, two broad anodic peaks are seen at 1.56 and 2.33 V, respectively, which diminish slightly in subsequent cycles, corresponding to extraction of  $\text{Li}^+$  from the  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  electrode, suggesting that charge storage is due to the intercalation of  $\text{Li}^+$  rather than a conversion reaction.<sup>[27]</sup> The cathodic and anodic peaks near 0.01 V correspond to lithiation/delithiation of the Super-P carbon.<sup>[49]</sup> In all subsequent cycles, broad and weak reversible peaks are observed at 0.89 and 1.00 V compared with those of  $\text{Li}^+/\text{Li}$  related to intercalation and deintercalation in the  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$ , respectively [Equation (1)]. **Figure S6** (supporting information) shows anodic (1.00 V) and cathodic (0.91 V) peaks indicating similar  $\text{Li}^+$  intercalation and deintercalation. Also, weak reversible peaks appear at 1.60 and 1.89 V vs.  $\text{Li}^+/\text{Li}$  during lithiation/delithiation process, respectively, tentatively ascribed to a possible reaction similar to that reported between  $\text{TiO}_2$  and lithiated titania [Equation (2)].<sup>[50]</sup>



As presented in **Figure 4b**, at  $30 \text{ mA g}^{-1}$ , the first charge and discharge capacities of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  for LIBs are 90 and 195  $\text{mAh g}^{-1}$  respectively. The large initial capacity loss likely arises for two reasons: (1) consumption of the electrolyte to form SEI and (2) irreversible reduction at the surface electrochemical active area. The 100<sup>th</sup> charge and discharge capacities of  $\text{Ti}_3\text{C}_2/\text{LiF}$  hybrids are 45 and 45  $\text{mAh g}^{-1}$  with a Columbic efficiency of 100 %. After long

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term cycling, the charge/discharge capacities of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  increase dramatically to 197 and 198  $\text{mAh g}^{-1}$ , a nearly 340 % capacity increase compared with the initial low capacity.  $\text{Ti}_3\text{C}_2$  from  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  contributes to the electrode capacities via intercalation/deintercalation reactions by tolerating the expansion/contraction of the interlayer distance during cyclic  $\text{Li}^+$  intercalation/deintercalation.<sup>[51-53]</sup> The decreasing lithium ion diffusion barriers and increasing  $\text{Li}^+$  storage capacities are significantly assigned to the expansion of  $\text{Ti}_3\text{C}_2$  interlayer spacing. Moreover, LiF used as etchant during preparation of  $m\text{-Ti}_3\text{C}_2/\text{LiF}$  sediments shows a reversible capacity of 20  $\text{mAh g}^{-1}$  at 100  $\text{mA g}^{-1}$  presented in **Figure S7** (supporting information), thus contributing a little to the capacity of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$ .

The cycling results at 150 and 600  $\text{mA g}^{-1}$  are presented in the **Figure 4d-e**. At 150  $\text{mA g}^{-1}$ ,  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  shows charge capacities of 74, 39, 59, 102, 151  $\text{mAh g}^{-1}$  and discharge capacities of 161, 39, 59, 102, 151  $\text{mAh g}^{-1}$  respectively at 1<sup>st</sup>, 200<sup>th</sup>, 400<sup>th</sup>, 600<sup>th</sup>, 900<sup>th</sup> cycles. Also, the charge/discharge profiles during the 1<sup>st</sup>, 200<sup>th</sup>, 400<sup>th</sup>, 600<sup>th</sup> and 900<sup>th</sup> cycles shown in **Figure 4c** are in good agreement with the results shown in **Figure 4d**. When the current density increases to 600  $\text{mA g}^{-1}$ , the capacities should decrease. In detail, the first charge and discharge capacities of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  are 54 and 106  $\text{mAh g}^{-1}$  respectively. With the capacities decreasing initially and then increasing, the 1000<sup>th</sup> charge and discharge capacities are 94 and 94  $\text{mAh g}^{-1}$  respectively, with a columbic efficiency of 100 %. By the 3000<sup>th</sup> charge and discharge, capacities both retain 91  $\text{mAh g}^{-1}$ .

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The cycling comparison (**Figure S8**) (supporting information) shows that the electrochemical performance of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  is much better than those of  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$  and  $\text{Ti}_3\text{C}_2$ . In detail, the capacities of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  and  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$  exhibit a common feature: decreasing initially, then gradually increasing and finally stabilizing with increasing cycle numbers, while the capacities of  $\text{Ti}_3\text{C}_2$  first decrease sharply, then decrease gradually. The charge capacities of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$ ,  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$  and  $\text{Ti}_3\text{C}_2$  after 1500 cycles are 136, 52 and 50  $\text{mAh g}^{-1}$  respectively at 300  $\text{mA g}^{-1}$ . The obvious distinction shows that LiF plays a significant role in increasing the capacity.

To determine the conductivity and ion transport properties, **Figure 4f** compares the Nyquist plots of  $\text{Ti}_3\text{C}_2$ ,  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  and  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$ . Each plot consists of two parts: a semicircle at high frequency and a straight line at low frequency, which correspond to charge transfer resistance ( $R_{\text{ct}}$ ) and Warburg impedance ( $W$ ) associated with  $\text{Li}^+$  diffusion in the bulk electrode.  $R_{\text{ct}}$  is a combination of the electrolyte-accessible area and electrical conductivity of the electrode. A larger electroactive surface area leads to lower  $R_{\text{ct}}$ . Apparently, the fitting results (**Figure 4g** and **Table S8**, supporting information) indicate that the semicircle diameter of  $\text{Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  matches an  $R_{\text{ct}}$  value of 33  $\Omega$ , lower than that of  $\text{Ti}_3\text{C}_2$  (127  $\Omega$ ) and  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$  (427  $\Omega$ ), indicating a lower charge transfer resistance. Nevertheless, the electronic resistance ( $R_s$ ) of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  (6.4  $\Omega$ ) stays in the middle of those of  $\text{Ti}_3\text{C}_2$  (9.5  $\Omega$ ) and  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$  (3.5  $\Omega$ ).

The diffusion coefficients of  $\text{Li}^+$  are calculated as follows:

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$$D_{Li^+} = \frac{R^2 T^2}{2 A^2 n^4 F^4 c^2 \sigma^2}$$

(3)

Here  $R$  is the gas constant ( $R=8.314 \text{ J mol}^{-1} \text{ K}^{-1}$ ),  $T$  is the absolute temperature ( $T=298 \text{ K}$ ),  $A$  is the polar area ( $A=1.13 \text{ cm}^2$ ),  $n$  is the number of electron transfers ( $n=1$ ) and  $F$  is the Faraday constant ( $F=96485 \text{ C mol}^{-1}$ ).  $c$  is the concentration of lithium ion electrolyte ( $c=1 \text{ mol L}^{-1}$ ). The calculated results are presented in **Table S8** (supporting information). The  $D_{Li^+}$  of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  ( $4.9 \times 10^{-16} \text{ cm}^2 \text{ s}^{-1}$ ) is higher than that for  $\text{Ti}_3\text{C}_2$  ( $3.4 \times 10^{-16} \text{ cm}^2 \text{ s}^{-1}$ ). These values are an order of magnitude greater than that of  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$  ( $5.5 \times 10^{-17} \text{ cm}^2 \text{ s}^{-1}$ ). The low diffusion rate for  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$  may arise from incomplete etching of the parent phase and the sluggish transport of  $\text{Mg}^{2+}$ . These results support the idea that  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  show better electrochemical performance due to introduction of extra LiF. Thus, LiF can effectively diffuse into the interlayer channels of  $\text{Ti}_3\text{C}_2$ , thereby achieving faster ion transfer than the sample etched by that without LiF.

CV was run for  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  electrode for LIBs at different sweep rates ( $0.1\text{-}0.8 \text{ mV s}^{-1}$ ) after 1000 cycles (**Figure 5a**) at  $300 \text{ mA g}^{-1}$  to explore the charge transfer mechanism of the materials. The logarithm of the sweep rate ( $v$ ) and peak current ( $i$ ) are linear through the following formula:

$$i = a v^b \Leftrightarrow \log i = b \log v + \log a$$

The magnitude of the slope  $b$  reflects control of the electrochemical reaction. When  $b = 0.5$ , the peak current exhibits a linear relationship with the square root of the sweep rate ( $v^{1/2}$ ),

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indicating that the reaction process is a typical diffusion-controlled battery storage process.

When  $b = 1$ , the peak current is proportional to the sweep rate, revealing capacitive-controlled energy storage behavior.<sup>[54-55]</sup> **Figure 5b** shows that the  $b$  values of the anodic (peak A) and cathodic (peak B) peaks are 0.90 and 0.89, suggesting that a capacitive-controlled energy storage mechanism cannot be ignored in the  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  electrodes.

On the basis of the relationship between current value ( $i(V)$ ) and fixed voltage ( $V$ ), the total capacitance contribution at a certain sweep rate can be quantified by the following equation through the separation of the specific capacitive ( $k_1v$ ) and diffusion control ( $k_2v^{1/2}$ ) contributions:

$$i(V) = k_1v + k_2v^{1/2} \Leftrightarrow i(V) / v^{1/2} = k_1v^{1/2} + k_2$$

The quantitative calculation results presented in **Figure 5c** and **S9** (supporting information) show that the capacitive contributions at 0.1, 0.2, 0.4, 0.6, 0.8  $\text{mV s}^{-1}$  are 55.9, 60.4, 68.2, 73.7 and 78.0 % respectively. Moreover, the proportion of capacitive-controlled capacity increases with increasing sweep rates (**Figure 5d**), indicating that the capacitive behavior is more useful for  $\text{Li}^+$  intercalation/deinteraction at higher sweep rates, owing to the rapid charge/discharge characteristic of the energy storage mechanism. The  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  successfully combine the dynamic equilibrium of fast capacitive-controlled pseudocapacitance and high diffusion-controlled energy storage, providing considerable electrochemical performance for LIBs.

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The *ex-situ* SEM images of fresh electrodes, electrodes after 200, 600, and 1200 cycles for  $\text{Ti}_3\text{C}_2$  and  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  at  $300 \text{ mA g}^{-1}$  are given in **Figure 6** respectively to verify the volume effect and structural stability of materials for LIBs. As displayed in **Figure 6a-d**, the fresh  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  electrode before cycling exhibits a longitudinal thickness of  $17.1 \mu\text{m}$ , where the operating electrodes after 200, 600, 1200 cycles increases slightly to 18.4, 19.4,  $20.1 \mu\text{m}$  respectively with a final expansion of 17.5 %.

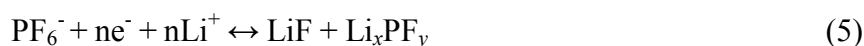
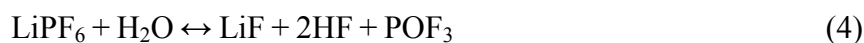
For comparison, the  $\text{Ti}_3\text{C}_2$  electrodes show one major increase in thickness, before cycling ( $13.5 \mu\text{m}$ , **Figure 6e**), after 200 cycles ( $20.2 \mu\text{m}$ , **Figure 6f**), after 600 cycles ( $20.9 \mu\text{m}$ , **Figure 6g**) and after 1200 cycles ( $22.1 \mu\text{m}$ , **Figure 6h**) with a expansion ratio of 63.7 %, thereby indicating the limitation in the volume change of the electrodes during cycling when LiF penetrates. Furthermore, **Figure S10** (supporting information) indicates that  $\text{Ti}_3\text{C}_2$  electrode surface exhibits cracks without LiF after 600 cycles at  $300 \text{ mA g}^{-1}$ , and even worse after 1200 cycles. These cracks lead to electrode polarization and effectiveness of the active material, thereby causing capacity fading and reducing battery cycling life. Interestingly, this phenomenon is not observed on the surfaces of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  electrodes during cycling.

*Ex-situ* XRD of fresh electrode, electrodes after 200, 600, 1200 cycles for  $\text{Ti}_3\text{C}_2$  in fully charged state are shown in **Figure 7a**. The characteristic planes, (002) and (004), shift dramatically to lower angle, as  $\text{Ti}_3\text{C}_2$  structure changes considerably during cycling. Nevertheless, when LiF present, the characteristic (002) and (004) planes (**Figure 7b**) exhibit no obvious shift with the increasing cycle numbers, demonstrating a negligible structural

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change with long term cycling. Overall, it implies that LiF prevents the electrode from expanding and cracking, enhancing  $\text{Ti}_3\text{C}_2$  performance in LIBs.

It is reasonable to propose a simple mechanism to explain the role of LiF during LIB cycling. Previous investigations suggest that electrode SEI in commercial LIBs is unstable and evolves over calendar life cycling,<sup>[35, 56]</sup> resulting in the changes in the SEI composition. The changes include typically an increase in the concentration of inorganic species such as LiF caused by primary side reactions shown in Equation (3)-(6).<sup>[35-36,57,58]</sup> First, the decomposition of the electrolyte accompanied by LiF generation occurs with difficulty owing to Le Chatelier's principle, hindering the SEI formation on  $\text{Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  electrode surfaces. Then the LiF in  $\text{Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  performs as an artificial SEI on the electrode (**Figure 7d**), creating shuttles for  $\text{Li}^+$  diffusion. Nevertheless, a simple  $\text{Ti}_3\text{C}_2$  electrode without LiF will see formation of an SEI induced by electrolyte decomposition during cycling (**Figure 7c**), causing the electrode to thicken and crack. LiF not only provides protective SEIs for the electrodes but also serves as a  $\text{Li}^+$  shuttle, enhancing the electrochemical performance during battery cycling to great extent.



Except for the “always discarded” sediments, **Figure 8a-b** indicate that single-layered

MXene (*s*- $\text{Ti}_3\text{C}_2$ ) collected from the supernatants shows a two-dimensional morphology. The

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XRD (**Figure 8c**) shows that (002) peak shifts to lower angle compared with  $\text{Ti}_3\text{AlC}_2$  (Fig. 1a) and (104) peak disappears, verifying the successful preparation of  $s\text{-Ti}_3\text{C}_2$ . When applied in LIBs,  $s\text{-Ti}_3\text{C}_2$  electrode shows a reversible capacity of  $194 \text{ mAh g}^{-1}$  at  $100 \text{ mA g}^{-1}$  after 100 cycles. When  $s\text{-Ti}_3\text{C}_2$  physically mixed with LiF powder at different weigh ratio,  $s\text{-Ti}_3\text{C}_2+\text{LiF}$  (20 wt. %) and  $s\text{-Ti}_3\text{C}_2+\text{LiF}$  (40 wt. %) electrodes show reversible capacities of 335 and 186  $\text{mAh g}^{-1}$  respectively (**Figure 8d**). Besides,  $s\text{-Ti}_3\text{C}_2+\text{LiF}$  (20 wt. %) electrode shows the highest coulombic efficiency of 83 % than  $s\text{-Ti}_3\text{C}_2$  (37 %) and  $s\text{-Ti}_3\text{C}_2+\text{LiF}$  (40 wt. %) (54 %) for first cycle. First, LiF in  $s\text{-Ti}_3\text{C}_2+\text{LiF}$  mixtures performs as an artificial SEI on the electrode, improving the initial coulombic efficiency and alleviating the capacity decaying during battery cycling. Also, LiF should create shuttles for  $\text{Li}^+$  diffusion, enhancing the electrochemical performance. On the other hand, excessive LiF will reduce capacity of the electrodes owing to the low capacity of LiF. Besides, the conductivity of the electrodes will be decreased to some extent when LiF added.<sup>[59]</sup> Thus, an appropriate amount of LiF is significant for the  $s\text{-Ti}_3\text{C}_2$  electrodes.

As a control set of studies, LiF (20 wt. %) was mixed separately with different materials including  $\text{Ti}_3\text{C}_2$ , anatase  $\text{TiO}_2$  and commercial tin (Sn) powder, and then assembled as electrodes for LIBs. **Figure S11** (supporting information) shows that the capacities of  $\text{Ti}_3\text{C}_2+\text{LiF}$  and  $\text{Ti}_3\text{C}_2$  are 168 and  $50 \text{ mAh g}^{-1}$  at  $300 \text{ mA g}^{-1}$  after 1500 cycles. Previous researches reported that there was a great volume change in the process of charge/discharge of tin anode ( $> 260\%$ ) for LIBs,<sup>[60-61]</sup> leading to a sharp decline in capacity. However, for Sn powder mixed with 20 wt. % LiF powder, **Figure S12** presents that reversible capacities of

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Sn+LiF are 158, 120, 40 mAh g<sup>-1</sup> respectively at 50, 100 and 500 mA g<sup>-1</sup>, which are greater than those of sole Sn (62, 41, 24 mAh g<sup>-1</sup> respectively). These results suggest that LiF can enhance the capacity of such kinds of materials typically found to undergo significant expansion during cycling in LIB formats. The volume change for anatase TiO<sub>2</sub> used in LIBs during cycling was less than 5 %.<sup>[62-64]</sup> **Figure S13** (supporting information) indicates that the reversible capacities of TiO<sub>2</sub> are 44, 35, 25 mAh g<sup>-1</sup> respectively at 50, 100 and 500 mA g<sup>-1</sup>, slightly less than those of TiO<sub>2</sub>+LiF (57, 40 and 37 mAh g<sup>-1</sup> respectively). These results further indicate that enhanced electrochemical performance can be mainly ascribed to the LiF penetration, especially for these materials undergoing great volume change during cycling.

### 3. Conclusion

Etching Ti<sub>3</sub>AlC<sub>2</sub> using HCl and LiF results in supernatants containing *s*-Ti<sub>3</sub>C<sub>2</sub> as end-products and *m*-Ti<sub>3</sub>C<sub>2</sub>/LiF sediments [*m*-Ti<sub>3</sub>C<sub>2</sub>/LiF(S<sub>1</sub>)] always discarded as “debris”. Ti<sub>3</sub>C<sub>2</sub> from *m*-Ti<sub>3</sub>C<sub>2</sub>/LiF(S<sub>1</sub>) sample presents book-like microstructures with some LiF impregnated into Ti<sub>3</sub>C<sub>2</sub>. LiF not only suppresses expansion of *m*-Ti<sub>3</sub>C<sub>2</sub>/LiF(S<sub>1</sub>) electrodes for LIBs during cycling but also increases capacities with increasing cycle numbers. The results confirm that LiF enhances the electrochemical properties, structural stability and ion migration rates. On the one hand, Ti<sub>3</sub>C<sub>2</sub> acts as a skeleton to accelerate electron and ion migration. On the other hand, LiF serves as a Li<sup>+</sup> transfer shuttle for insertion and extraction, forming a stable artificial SEI to prevent electrolyte and electrode degradation, thereby integrating the merits of

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both components. Also,  $\text{Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  possess superior high-rate and long-term cycling performance due to pseudocapacitance. Besides,  $s\text{-Ti}_3\text{C}_2+\text{LiF}$  (20 wt. %) shows considerable initial coulombic efficiency and reversible capacity. Thus, the introduction of LiF can be a simple and efficient route paving the way to enhance the electrochemical performance for LIBs, as well as reducing cost of synthesis for MXene by making full use of the sediments.

### Supporting Information

Supporting Information is available from the Wiley Online Library or from the author.

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Figures and captions

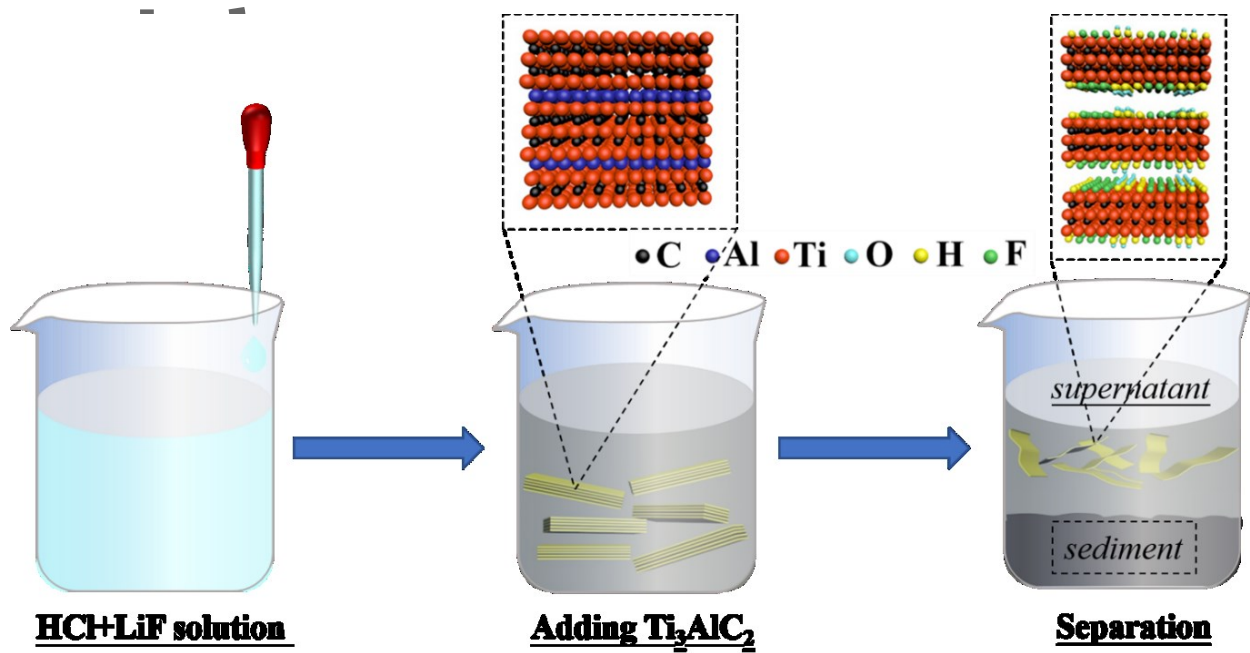
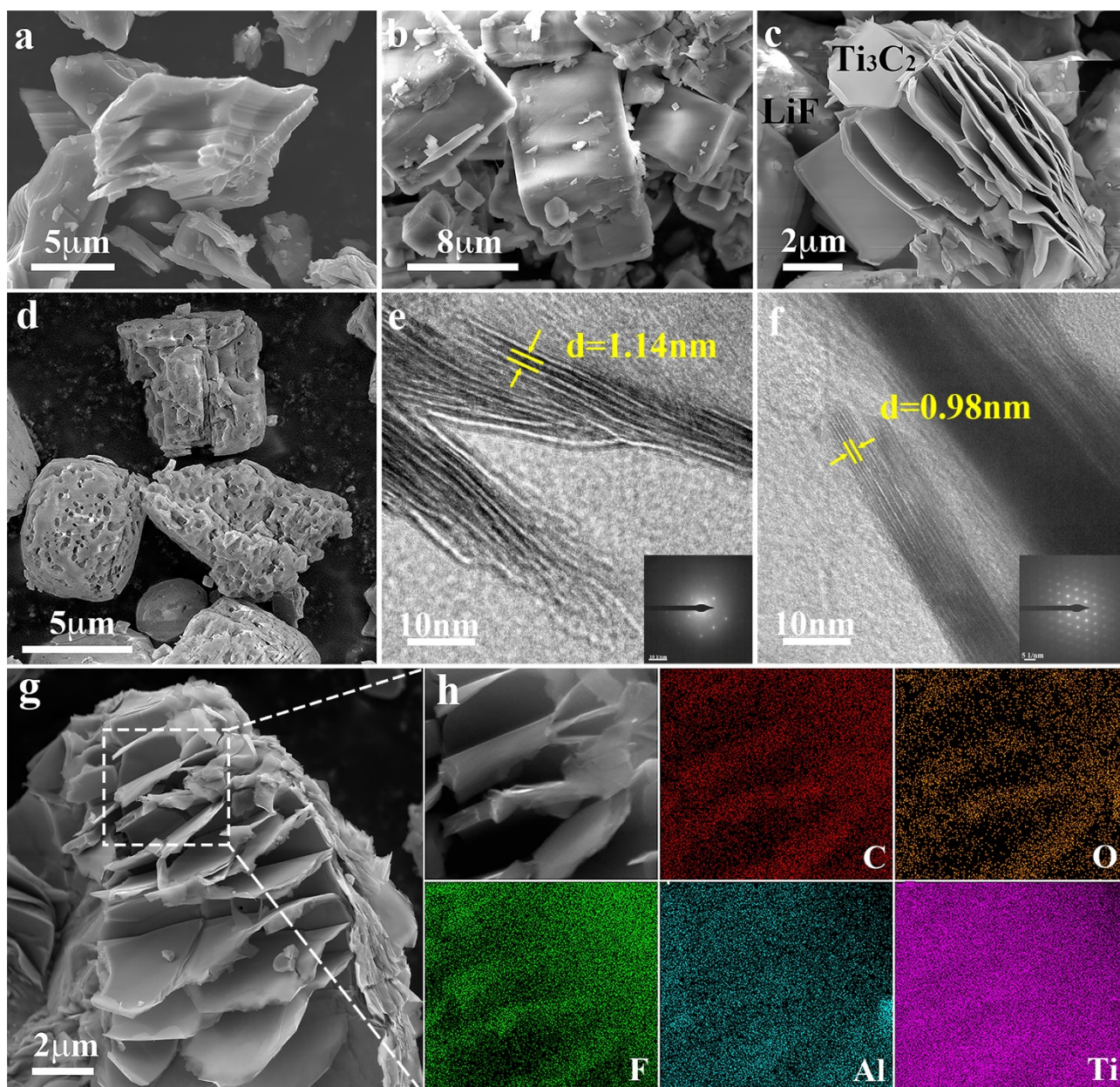
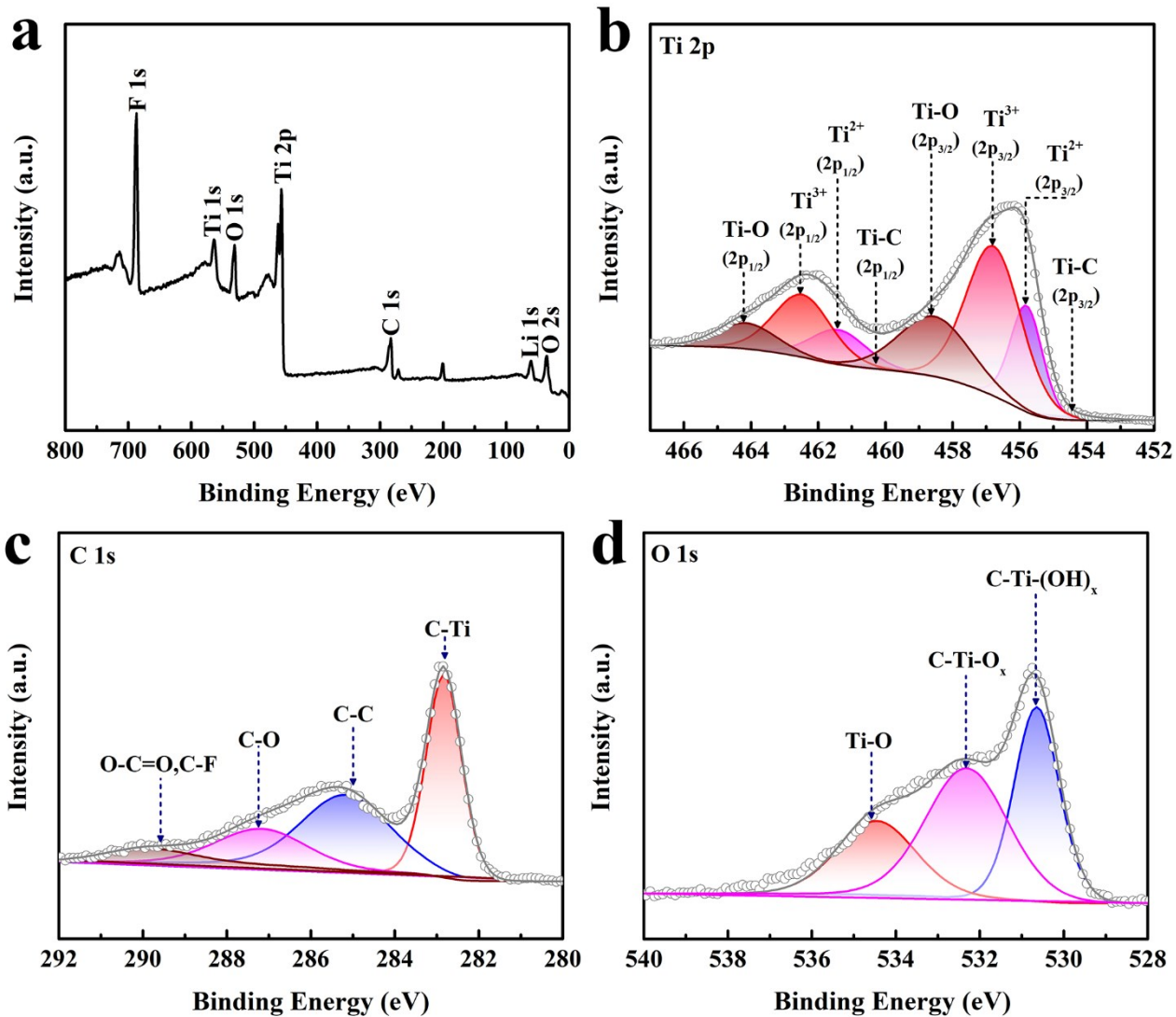


Figure 1. General methods used to prepare  $m-Ti_3C_2/LiF$  sediments.

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**Figure 2.** SEM of a)  $\text{Ti}_3\text{AlC}_2$ , b) LiF before etching, c)  $m\text{-Ti}_3\text{C}_2$  etched by HCl+LiF, d) LiF after etching. HRTEM image (inset is SAED image) of e)  $m\text{-Ti}_3\text{C}_2$  etched by HCl+LiF and f)  $\text{Ti}_3\text{C}_2$  etched by HF. g-h) SEM and EDX of  $m\text{-Ti}_3\text{C}_2$  etched by HCl+LiF.

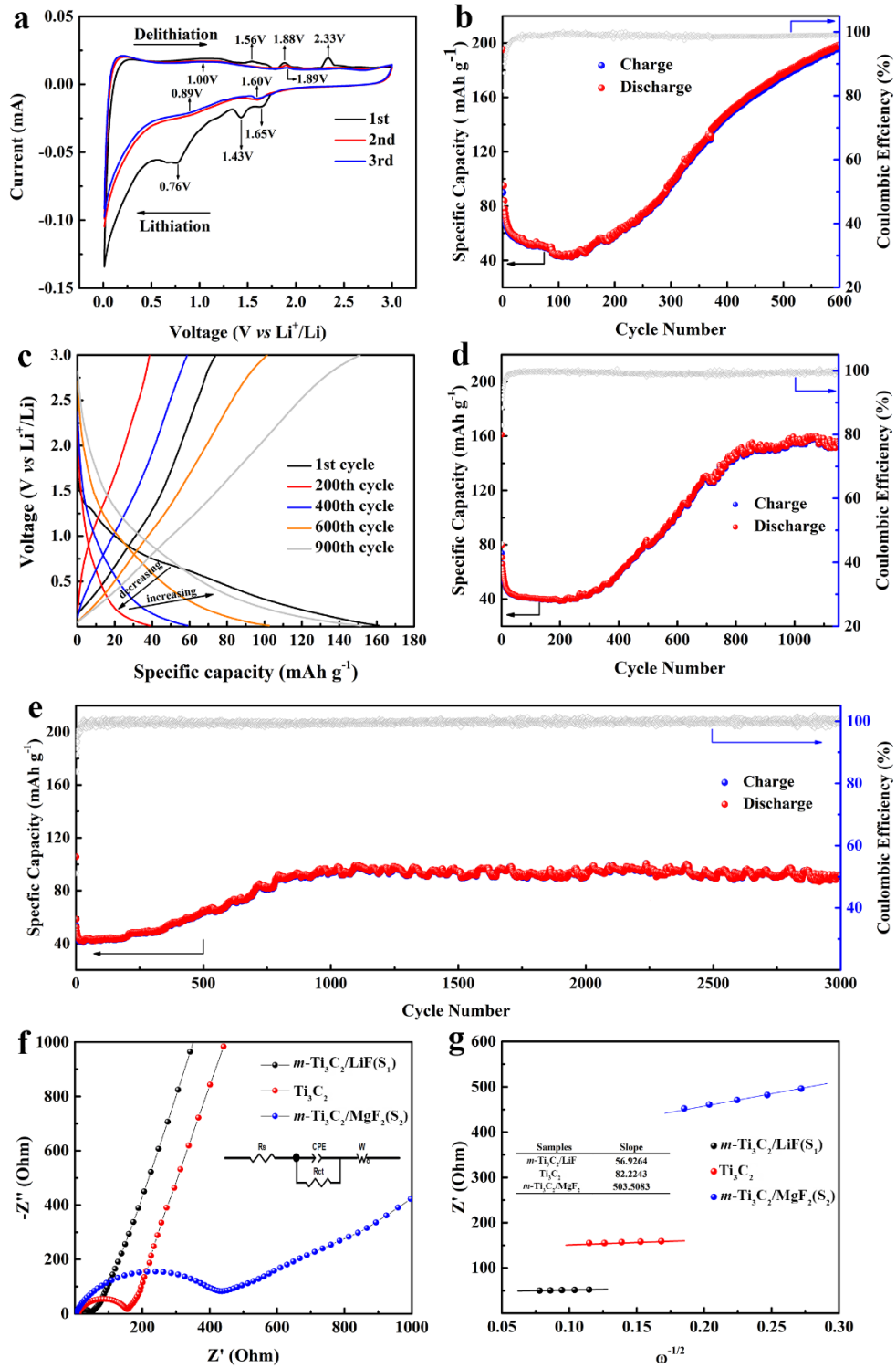


**Figure 3.** XPS spectra of the *m*-Ti<sub>3</sub>C<sub>2</sub>/LiF(S<sub>1</sub>). a) Survey spectrum, b) Ti 2p, c) C 1s and d) O

1s.

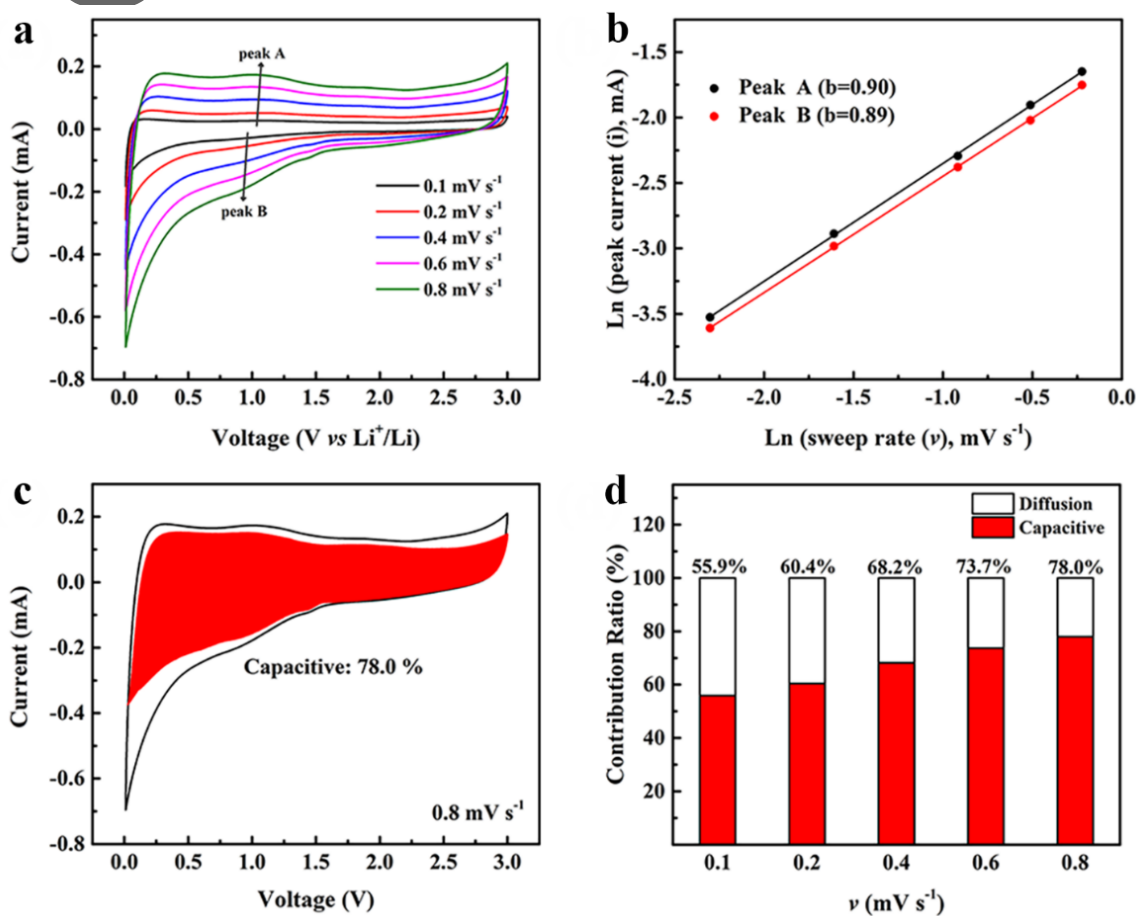
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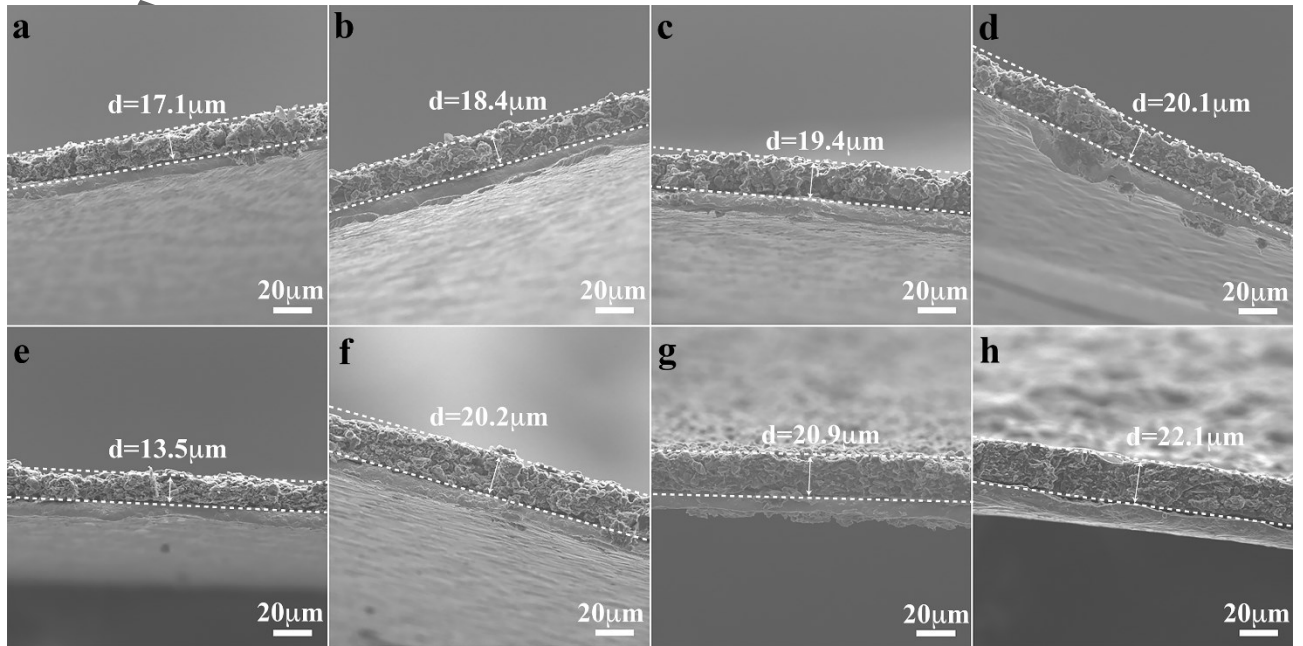
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**Figure 4.** Electrochemical evaluation of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$ . a) CV curves at  $0.1\text{ mV s}^{-1}$  for the first three cycles, Long term cycling performance at b) 30, d) 150, e) 600  $\text{mA g}^{-1}$ , c) and charge/discharge profiles during the 1<sup>st</sup>, 200<sup>th</sup>, 400<sup>th</sup>, 600<sup>th</sup> and 900<sup>th</sup> cycles at  $150\text{ mA g}^{-1}$ . f) Electrochemical impedance spectra (inset is equivalent circuit diagram) and g) Linear fitting  $Z'$  vs.  $\omega^{-1/2}$  in the low-frequency region of  $\text{Ti}_3\text{C}_2$ ,  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  and  $m\text{-Ti}_3\text{C}_2/\text{MgF}_2(\text{S}_2)$ .



**Figure 5.** Kinetic analyses of electrochemical behavior for LIBs. a) CV curves of  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  electrode at various sweep rates from  $0.1$  to  $0.8\text{ mV s}^{-1}$  after 1000 cycles. b) Relationship between peak currents and sweep rates (plotted with natural logarithm axis). c)

CV curve with corresponding capacitive contribution at  $0.8 \text{ mV s}^{-1}$ . d) Capacitive contribution ratios at different sweep rates.

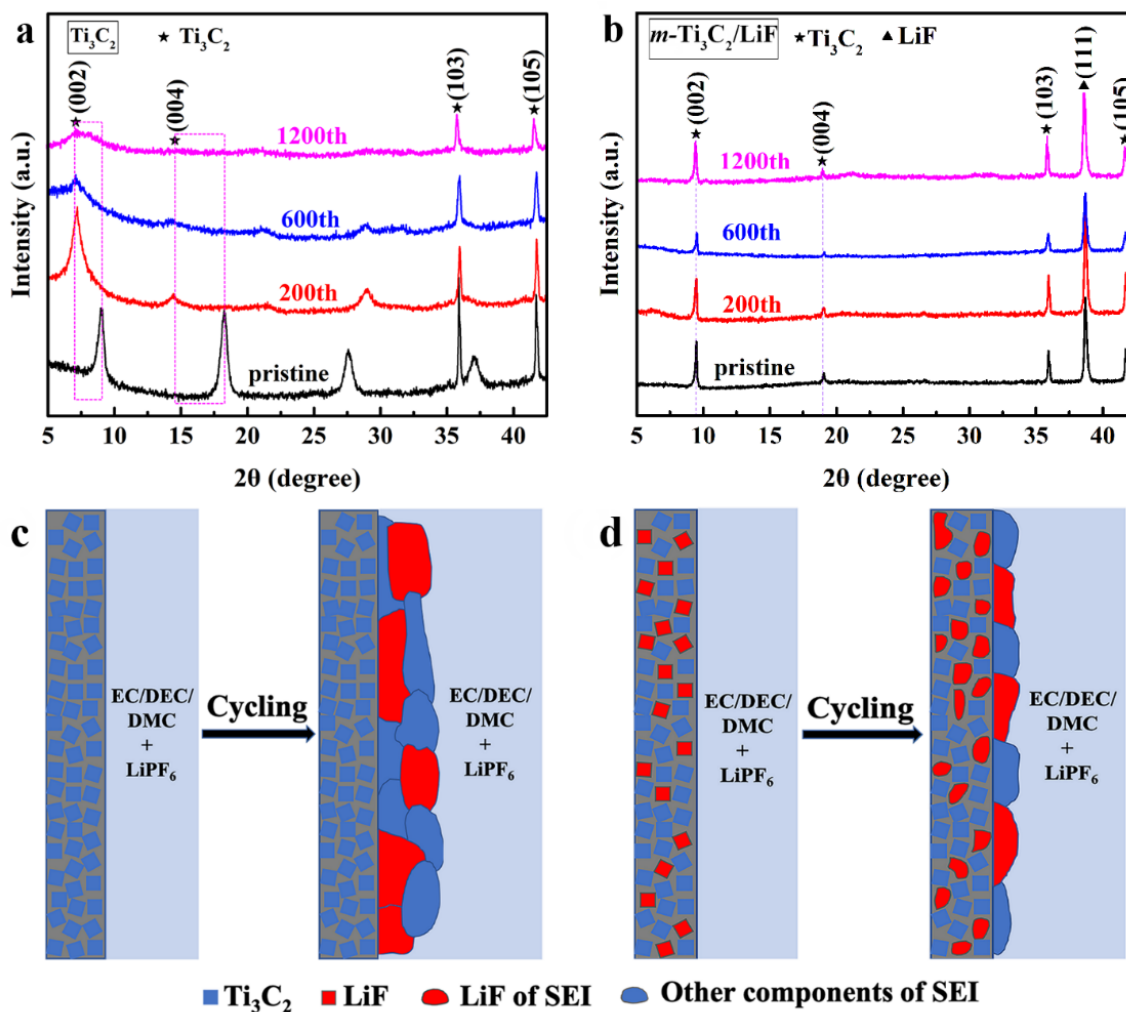


**Figure 6.** Cross sectional SEM images of the electrodes for LIBs in fully charged state. a)

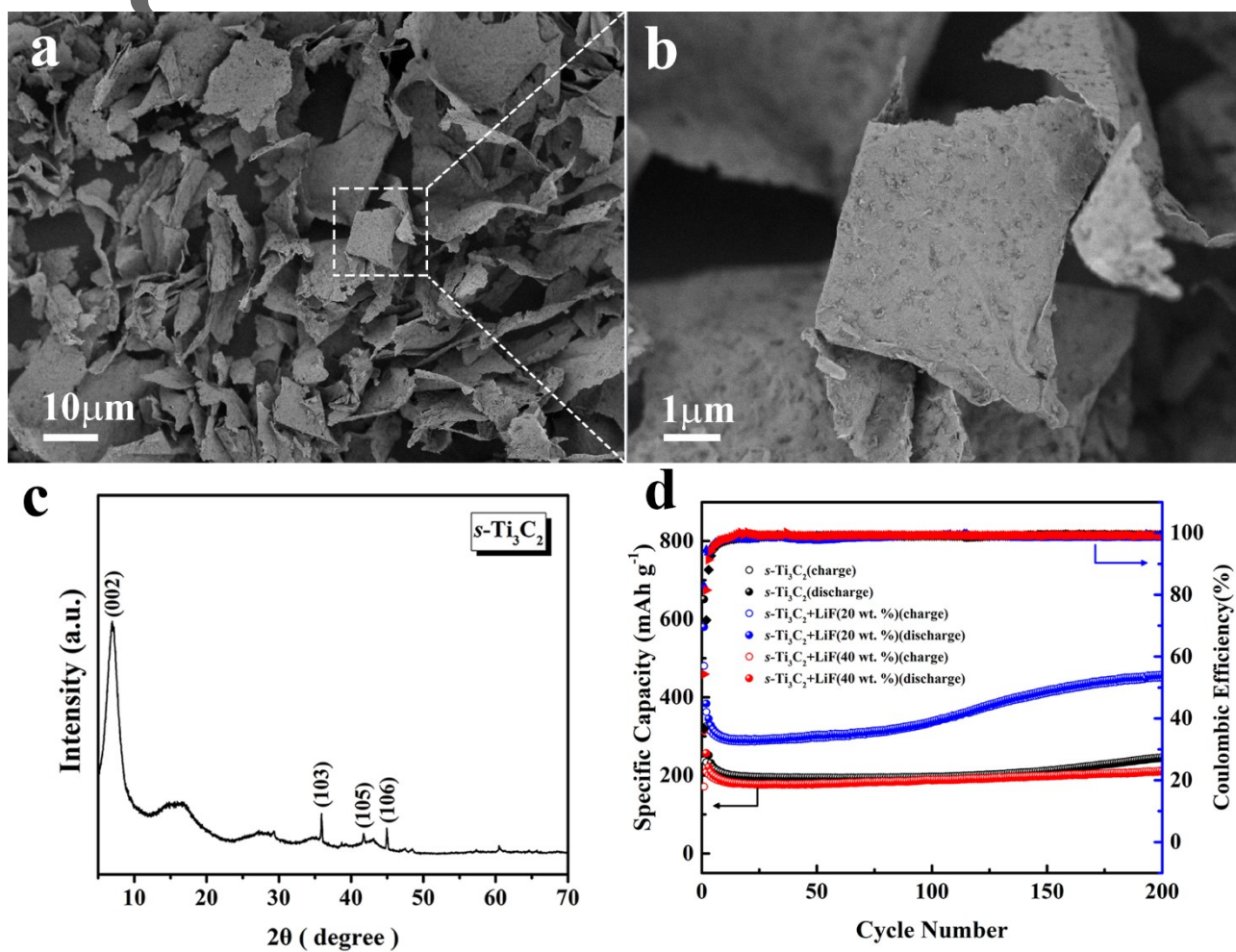
Fresh electrode, electrodes after b) 200, c) 600, d) 1200 cycles at  $300 \text{ mA g}^{-1}$  for

$m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$ . e) Fresh electrode, electrodes after f) 200, g) 600, h) 1200 cycles at  $300 \text{ mA}$

$\text{g}^{-1}$  for  $\text{Ti}_3\text{C}_2$ .



**Figure 7.** *Ex-situ* XRD of the electrodes in fully charged state. a) Fresh electrode, electrodes after 200, 600 and 1200 cycles at  $300\text{mA g}^{-1}$  for  $\text{Ti}_3\text{C}_2$ , b) Fresh electrode, electrodes after 200, 600 and 1200 cycles at  $300\text{mA g}^{-1}$  for  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$ . Conceptual schemes of SEI formation for electrolytes containing EC/DEC/DMC and  $\text{LiPF}_6$  on the electrodes of c)  $\text{Ti}_3\text{C}_2$  and d)  $m\text{-Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$ .



**Figure 8.** a-b) SEM of  $s\text{-Ti}_3\text{C}_2$  from the supernatant at different scales. c) XRD of  $s\text{-Ti}_3\text{C}_2$ . d) Cycling performance of  $s\text{-Ti}_3\text{C}_2$ ,  $s\text{-Ti}_3\text{C}_2+\text{LiF}$  (20 wt. %) and  $s\text{-Ti}_3\text{C}_2+\text{LiF}$  (40 wt. %) at  $100\ \text{mA g}^{-1}$  for LIBs.

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**Insert Table of Contents Artwork**

Etching  $\text{Ti}_3\text{AlC}_2$  using HCl and LiF results in the *m*- $\text{Ti}_3\text{C}_2/\text{LiF}$  sediments always discarded as "debris" and the supernatants containing *s*- $\text{Ti}_3\text{C}_2$ , further to be investigated in lithium ion batteries. The *m*- $\text{Ti}_3\text{C}_2/\text{LiF}(\text{S}_1)$  electrodes show negative capacity fading with capacity increasing to  $198 \text{ mAh g}^{-1}$  (600<sup>th</sup> cycle) at  $30 \text{ mA g}^{-1}$  while *s*- $\text{Ti}_3\text{C}_2+\text{LiF}(40 \text{ wt. \%})$  electrodes display a reversible capacity of  $335 \text{ mAh g}^{-1}$  (100<sup>th</sup> cycle) at  $100 \text{ mA g}^{-1}$ . LiF takes a significant role in electrochemical performance enhancing.

**Keyword**

$\text{Ti}_3\text{C}_2$ ; MXene; LiF; lithium ion batteries; capacity increasing

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**Title**

**Turning Trash into Treasure: MXene with Intrinsic LiF Solid Electrolyte Interfaces Performs Better and Better during Battery Cycling**

