

Department of Applied Mechanics and Engineering Science, University of Michigan, Ann Arbor, Mich. (U.S.A.) and  
 School of Mathematical Sciences, Flinders University, Bedford Park, S.A. (Australia)

## Upper and lower bounds for the pressure error in the rectilinear flow along a slot with a pressure gradient

K. R. Rajagopal and R. R. Huilgol

With 6 figures

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### 1. Introduction

Viscometric flows, locally equivalent to simple shearing, are very important in the theory of incompressible viscoelastic fluids. It is well known, e.g. see the review article by Pipkin and Tanner (1), that in these flows, the two normal stress differences  $N_1$  and  $N_2$  and the shear stress function  $\tau$  play crucial roles. With respect to a local Cartesian system, if  $v = \kappa y i$  is the velocity field, then  $N_1$ ,  $N_2$  and  $\tau$  are defined through:

$$N_1 = T\langle xx \rangle - T\langle yy \rangle, \quad [1.1]$$

$$N_2 = T\langle yy \rangle - T\langle zz \rangle, \quad [1.2]$$

$$\tau = T\langle xy \rangle, \quad [1.3]$$

$$N_i = N_i(\kappa), \quad i = 1, 2; \quad \tau = \tau(\kappa), \quad [1.4]$$

$$N_i(\kappa) = N_i(-\kappa), \quad i = 1, 2; \quad \tau(-\kappa) = -\tau(\kappa). \quad [1.5]$$

In [1.1]–[1.3],  $T\langle ij \rangle$  are the physical components of the stress tensor  $T$  and in [1.4]–[1.5],  $\kappa$  is called the rate of shear. Much work, theoretical and experimental, has been done in determining the various configurations wherein  $N_1$ ,  $N_2$  and  $\tau$  may be measured. For example, apart from Pipkin and Tanner (1), one may consult Lodge (2), or Huilgol (3), or Walters (4) for an exhaustive study of these aspects. This would reveal that in a number of situations, measurement of the stress distribution on a flat plate (e.g. in cone and plate flow, torsional flow) or at a point on a curved surface (e.g. in Couette flow) are required. One approach to the measurement is to drill a hole or cut a slot for the insertion of a pressure sensitive device. The question this raises is: does the presence of a hole induce errors in the values of the stresses so recorded?

Twenty-five years ago, Greensmith and Rivlin (5) did a number of tests to determine whether the holes would induce “pressure-hole errors”. They concluded, by varying the diameters of holes, that these errors did not exist. The matter rested here until Adams and Lodge (6) found that the normal stress measurements obtained from the cone-and-plate apparatus did not agree with those obtained from the parallel-plate apparatus.

Following upon this discovery, Broadbent et al. (7) published an article in which they pointed out that if a systematic error,  $p_e$ , independent of the hole size but dependent on the shear stress  $\tau$ , was assumed to exist, then these inconsistencies could be resolved. These authors found an equation connecting  $p_e$  and  $\tau$ , which was somewhat empirical.

The next advance was made by Tanner and Pipkin (8), who considered the creeping flow of an incompressible second order fluid (Coleman and Noll (9)) across an infinitely deep slot. They found that

$$p_e = -N_1(\kappa)/4, \quad [1.6]$$

where for the second-order fluid, described by:

$$T + p\mathbf{1} = \eta_0 A_1 + \beta A_1^2 + \gamma A_2, \quad [1.7]$$

with  $\eta_0$ ,  $\beta$  and  $\gamma$  constants,  $A_1$  and  $A_2$  being the first two Rivlin-Ericksen (10) tensors,

$$N_1(\kappa) = -2\gamma\kappa^2. \quad [1.8]$$

Using this very constitutive relation [1.7], Kearsley (11) found that in the creeping, rectilinear flow along a deep slot,

$$p_e = N_2(\kappa)/2, \quad [1.9]$$

$$N_2(\kappa) = (\beta + 2\gamma)\kappa^2. \quad [1.10]$$

Later, *Kearsley* (12) discussed the rectilinear motion of the second-order fluid between two infinitely parallel plates  $D$  apart, with the top plate moving with a constant speed  $V$  and the bottom plate at rest. The bottom plate had a slot, of finite depth  $d$  and width  $W$ , in the direction of the motion. *Kearsley* obtained an exact solution to this problem and found explicitly that

$$p_e = \frac{N_2(\kappa)}{2} \cdot G(k, \alpha), \tag{1.11}$$

where  $N_2(\kappa)$  is evaluated at  $\kappa = V/D$ , and

$$G(k, \alpha) = \frac{1 - k^2}{1 - k^2 \operatorname{sn}^2 \alpha} \tag{1.12}$$

with  $k$  and  $\operatorname{sn} \alpha$  being the *modulus* and *modular sine* respectively.

In this paper, we study the above problem of the rectilinear flow when along with the moving top plate, a constant pressure gradient  $c$  exists in flow direction. We have not been able to solve the problem completely; however, we have obtained upper and lower bounds to the error  $p_e$ . By putting  $c = 0$ , we can recover bounds for the case considered by *Kearsley* (12). A comparison with his solution (see fig. 4) has been made to indicate the position of the bounds relative to the exact values. If we put  $V = 0$ ,  $c \neq 0$ , then our results should be applicable to the ‘‘Omega flow’’ considered more recently by *Lobo* and *Osmers* (13) to measure  $N_1$ .

In this paper, we assume that  $N_2(\kappa) \leq 0$ .

### 2. Formulation of the problem

We are interested in the determination of the velocity field, in a Cartesian frame:

$$\dot{x} = 0, \quad \dot{y} = 0, \quad \dot{z} = w(x, y). \tag{2.1}$$

This steady flow takes place between a fixed bottom plate with a longitudinal slot which is along the direction of the flow, and a moving upper plate. Both plates are assumed to be infinitely long and wide, and the upper plate moves in the  $z$ -direction with a constant speed  $V$ . There is also a uniform pressure gradient  $\partial p / \partial z = \eta_0 c$  as well, where  $c \leq 0$  is a constant. The continuity equation is trivially satisfied and the equations of motion imply that  $w$  satisfies

$$\Delta w = c, \tag{2.2}$$

when body forces are ignored and the constitutive eq. [1.7] is used. In eq. [2.2]  $\Delta$  is the two-dimensional Laplacian:

$$\Delta = \frac{\partial^2}{\partial x^2} + \frac{\partial^2}{\partial y^2}. \tag{2.3}$$

The boundary conditions (see fig. 1) are:

$$w = \left\{ \begin{array}{l} V \text{ on } y = d + D; \\ 0, |x| \leq (W/2); y = 0; \\ 0, |x| = (W/2); 0 \leq y \leq d; \\ 0, |x| \geq (W/2); y = d; \\ w \rightarrow w(y) \text{ as } |y| \rightarrow \infty. \end{array} \right\} \tag{2.4}$$

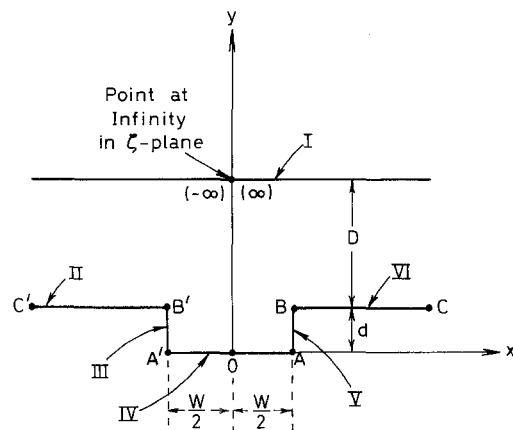


Fig. 1. Flow domain in the  $z$ -plane and the boundary regions I, II, III, IV, V and VI

We shall digress a little and note that the corresponding problem for a Newtonian fluid, i.e., the fluid defined by [1.7] with  $\beta = \gamma = 0$ , is also given by eqs. [2.1]–[2.4]. Thus the Newtonian and second-order fluid velocity fields are identical, but the pressure fields are not. In the Newtonian fluid,  $p^0 = p^0(z)$ , while in the second-order fluid, as shown by *Kearsley* (11), the pressure  $p$  is given in the steady flow [2.1] by:

$$p = p^0 - (\beta + 2\gamma) \frac{1}{\eta_0} \frac{dp^0}{dz} w, \tag{2.5}$$

i.e., by

$$p = p^0 - c(\beta + 2\gamma)w. \tag{2.6}$$

Using eqs. [1.7], [2.1] and [2.6], one can calculate the normal stress  $T_{yy}$  to be:

$$T_{yy} = -p^0 + \frac{1}{2}(\beta + 2\gamma) [(w_{,x}^2 - w_{,y}^2) - 2cw], \tag{2.7}$$

where the comma denotes the partial derivative and  $w_{,x}^2 = (\partial w/\partial x)^2$ , etc.

We assume that in this flow, the normal stress is measured at  $x = 0, y = 0$ , while the undisturbed normal stress, i.e., the true normal stress, is the one at  $x = \pm\infty, y = d$ . The pressure error  $p_e$  is then defined through:

$$p_e = T_{yy}(\pm\infty, d) - T_{yy}(0, 0). \tag{2.8}$$

Now, along the fixed plate,  $w = 0$  and  $w_{,x} = 0$  as well. Therefore, eqs. [2.7]–[2.8] lead to (12):

$$p_e = \frac{\beta + 2\gamma}{2} \cdot [w_{,y}^2(\pm\infty, d) - w_{,y}^2(0, 0)]. \tag{2.9}$$

If we calculate the second normal-stress difference for this fluid based on the shear rate at  $x = \pm\infty, y = d$ , and denote this by  $\bar{N}_2$ , [2.9] becomes:

$$p_e = \frac{1}{2} \bar{N}_2 G, \tag{2.10}$$

where

$$G = \left[ 1 - \frac{w_{,y}^2|_0}{w_{,y}^2|_C} \right]. \tag{2.11}$$

Here 0 denotes the origin and C denotes the point at  $(\infty, d)$  as shown in figure 1.

To sum up, the determination of  $p_e$  reduces to that of finding the function  $G$ , which depends on the dimensions of the flow:  $d, D, W$  as well as  $V$  and  $c$ .

**3. Bounds for the error**

If the solution of the Poisson's eq. [2.2], subject to the boundary conditions [2.4] is obtained, then  $G$  will be known. This is a formidable task because the conformal mapping which transforms the region in figure 1 – hereafter called the  $z$ -plane which should not be confused with the Cartesian co-ordinate – onto the upper half-plane in the  $\zeta$ -plane is given by (Carter (14)) a cumbersome result:

$$\frac{dz}{d\zeta} = M \left( \frac{1 - k^2 \zeta^2}{1 - \zeta^2} \right)^{1/2} \frac{1}{1 - k^2 \zeta^2 \operatorname{sn}^2 \alpha}. \tag{3.1}$$

We have already introduced the parameter  $k$  and  $\operatorname{sn} \alpha$  in eq. [1.12] above, and  $M$  is the Schwarz-Christoffel constant to be determined. (The Appendix treats these matters in a more detailed fashion to which the reader is referred). Having accomplished this mapping, the usual procedure is to map this upper half-plane onto

a unit circle in the  $\gamma$ -plane (fig. 3b), say, and determine the mapping:

$$z = \sum_{n=0}^{\infty} a_n \gamma^n. \tag{3.2}$$

If one finds the coefficients  $a_n$ , there still remains the task of solving the Poisson's equation in the  $\gamma$ -plane, which will now be  $\Delta w = f(\gamma_1, \gamma_2)$  rather than  $\Delta w = c$ . These remarks indicate why we have sought to obtain bounds for the solution to  $w$  and hence derive bounds for  $G$  itself.

To achieve these bounds, let us decompose  $w$ :

$$w = w_0 + w_1, \tag{3.3}$$

where  $w_0$  obeys:

$$\Delta w_0 = c, \tag{3.4}$$

and

$$w_0 = \begin{cases} V, & y = d + D \\ 0, & y = d. \end{cases} \tag{3.5}$$

The solution is trivially shown to be:

$$w_0 = \frac{c}{2} y^2 + by + e, \tag{3.6}$$

where  $b$  and  $e$  are the two constants:

$$b = \frac{V}{D} - \frac{c}{2}(D + 2d), \tag{3.7}$$

$$e = \frac{cd}{2}(d + D) - \frac{Vd}{D}. \tag{3.8}$$

Breaking up figure 1 into regions I, II, III, IV, V und VI, we can show that  $w_1$  satisfies:

$$\Delta w_1 = 0, \tag{3.9}$$

$$w_1 = \left\{ \begin{array}{l} 0, \text{ on I, II and VI,} \\ -\frac{c}{2}y^2 - by - e \text{ on III and V,} \\ -e \text{ on IV.} \end{array} \right\} \tag{3.10}$$

$$w_1 \rightarrow 0 \text{ as } |x| \rightarrow \infty,$$

so that  $w \rightarrow w_0$  as  $|x| \rightarrow \infty$ . Next, the constants  $c$  and  $V$  are such that  $c \leq 0$  and  $V \geq 0$ . From this, one obtains that  $b \geq 0$  and  $e \leq 0$  and using these it can be shown that the boundary data for  $w_1$  is non-negative. We shall now introduce two other harmonic functions  $w_1^L$  and  $w_1^U$ . These obey:

$$\Delta w_1^L = 0, \quad \Delta w_1^U = 0. \tag{3.11}$$

The boundary data for  $w_1^L$  and  $w_1^U$  are:

$$\begin{aligned}
 w_1^L &= \begin{cases} -e & \text{on IV} \\ 0 & \text{elsewhere,} \end{cases} \\
 w_1^L &\rightarrow 0 \text{ as } |x| \rightarrow \infty, \\
 w_1^U &= \begin{cases} -e & \text{on III, IV and V} \\ 0 & \text{elsewhere,} \end{cases} \\
 w_1^U &\rightarrow 0 \text{ as } |x| \rightarrow \infty.
 \end{aligned}
 \tag{3.12}$$

We claim that  $w_1^L < w_1 < w_1^U$ . To make this transparent, consider the mapping of the upper half of the  $\zeta$ -plane (fig. 2) onto the unit circle in the  $\gamma$ -plane, (see fig. 3), together with

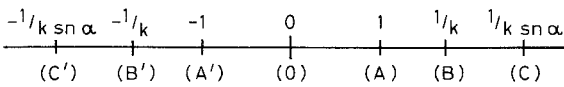


Fig. 2. Points in the  $\zeta$ -plane corresponding to the flow domain

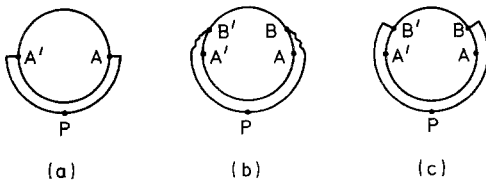


Fig. 3. Boundary data for  $w_1^L$ ,  $w_1$  and  $w_1^U$  in the  $\gamma$ -plane

the relevant boundary data for  $w_1^L$ ,  $w_1$  and  $w_1^U$ . Clearly, the functions  $(w_1 - w_1^L)$  and  $(w_1^U - w_1)$  are harmonic and the boundary data are non-negative. Hence, by the maximum principle (Protter and Weinberger (15)):

$$w_1^L < w_1 < w_1^U
 \tag{3.13}$$

as asserted.

Moreover, at the point  $P$  in the  $\gamma$ -plane which corresponds to 0 in the  $z$ -plane,

$$\begin{aligned}
 \frac{\partial}{\partial \gamma_2} (w_1^U - w_1) &\geq 0, \\
 \frac{\partial}{\partial \gamma_2} (w_1 - w_1^L) &\geq 0.
 \end{aligned}
 \tag{3.14}$$

A glance at eq. [3.1] shows that these mappings are all conformal at  $z = 0$  and hence

$$\frac{\partial w_1^U}{\partial y} \geq \frac{\partial w_1}{\partial y} \geq \frac{\partial w_1^L}{\partial y} \text{ at } 0.
 \tag{3.15}$$

Now, by the nature of the boundary conditions on  $w_1^L$  and  $w_1^U$ ,  $w_{1,x}^L \rightarrow 0$ ,  $w_{1,x}^U \rightarrow 0$  at  $|x| \rightarrow \infty$ .

Moreover, as we shall see,  $w_{1,y}^L \rightarrow 0$ ,  $w_{1,y}^U \rightarrow 0$  as  $|x| \rightarrow \infty$ . Bearing in mind the fact that  $w_{1,x} \rightarrow 0$  as  $|x| \rightarrow \infty$ , as well as the ellipticity of the problem with boundary data prescribed over a small region near the origin in the  $z$ -plane, one has that  $w_{1,y} \rightarrow 0$  as  $|x| \rightarrow \infty$  as well.

We shall now proceed to calculate  $w_{1,y}^L$  and  $w_{1,y}^U$ . This part is straightforward because  $w_1^L$  and  $w_1^U$  are harmonic with constant boundary data over  $(-1, 1)$  and  $(-1/k, 1/k)$ , respectively, in the  $\zeta$ -plane. Thus (for full details, see Rajagopal (16)):

$$\begin{aligned}
 \frac{\partial w_1^L}{\partial y} &= -\frac{e}{M\Pi} \left[ \left( \frac{1 - \zeta^2}{1 - k^2 \zeta^2} \right)^{1/2} \right. \\
 &\quad \cdot \left( \frac{1 - k^2 \zeta^2 \sin^2 \alpha}{\zeta^2 - 1} \right) + \left( \frac{1 - \bar{\zeta}^2}{1 - k^2 \bar{\zeta}^2} \right)^{1/2} \\
 &\quad \left. \cdot \left( \frac{1 - k^2 \bar{\zeta}^2 \sin^2 \alpha}{\bar{\zeta}^2 - 1} \right) \right],
 \end{aligned}
 \tag{3.16}$$

$$\begin{aligned}
 \frac{\partial w_1^U}{\partial y} &= -\frac{ek}{M\Pi} \left[ \left( \frac{1 - \zeta^2}{1 - k^2 \zeta^2} \right)^{1/2} \right. \\
 &\quad \cdot \left( \frac{1 - k^2 \zeta^2 \sin^2 \alpha}{\zeta^2 k^2 - 1} \right) + \left( \frac{1 - \bar{\zeta}^2}{1 - k^2 \bar{\zeta}^2} \right)^{1/2} \\
 &\quad \left. \cdot \left( \frac{1 - k^2 \bar{\zeta}^2 \sin^2 \alpha}{\bar{\zeta}^2 k^2 - 1} \right) \right],
 \end{aligned}
 \tag{3.17}$$

where  $\bar{\zeta}$  is the conjugate of  $\zeta$ . Note that when  $\zeta = \pm 1/k \sin \alpha$ , which corresponds to the point  $|x| \rightarrow \infty$  in the  $z$ -plane, these derivatives vanish.

Now, let us obtain the upper and lower bounds to  $w$  itself as:

$$w^U = w_0 + w_1^U, \quad w^L = w_0 + w_1^L.
 \tag{3.18}$$

Then, from the foregoing

$$\left. \begin{aligned}
 w_{,y}|_0 &= \frac{2ek}{M\Pi} + b, \quad w_{,y}|_0 = \frac{2e}{M\Pi} + b, \\
 w_{,y}|_c &= w_{,y}|_c = cd + b.
 \end{aligned} \right\}
 \tag{3.19}$$

We now define two functions  $G_1$  and  $G_2$  as:

$$G_1 = 1 - (w_{,y}|_0)^2 / (cd + b)^2,
 \tag{3.20}$$

$$G_2 = 1 - (w_{,y}|_0)^2 / (cd + b)^2.
 \tag{3.21}$$

Though, as we have shown,  $w_{,y}|_0 \leq w_{,y}|_0$ , it need not be true that  $G_1 \leq G_2$  always, because the squares of these derivatives are included in [3.20]–[3.21]. However, it will always be true that one of the following inequalities holds for the function  $G$  defined in [2.10]:

$$G_1 \leq G \leq G_2, \quad \text{or} \quad G_2 \leq G \leq G_1.
 \tag{3.22}$$

Bearing in mind that  $\bar{N}_2 \leq 0$ , one can obtain bounds for  $p_e$ , as defined in [2.11], by a correct choice of one of the inequalities in [3.22].

4. Results and discussion

For values of  $d/W \leq 0.7$ , we have found by direct calculation that  $w_{,y|0}^L > 0$  when  $D/W = 0.5$  and the parameter  $T$  (see [4.3] below) lies between 0 and 0.5. Because  $w_{,y|0}^L > 0$ , we have the result  $(w_{,y|0}^U)^2 > (w_{,y|0}^L)^2$ , and therefore  $G$  satisfies:

$$G_1 \leq G \leq G_2, \tag{4.1}$$

and because  $\bar{N}_2 \leq 0$ ,

$$\frac{\bar{N}_2 G_2}{2} \leq p_e \leq \frac{\bar{N}_2 G_1}{2}. \tag{4.2}$$

To facilitate the presentation of the results, we introduce a parameter  $T$  through

$$T = cD/\kappa_0, \quad \kappa_0 = V/D, \tag{4.3}$$

where  $\kappa_0$  is a measure of the shear rate. Thus  $G_1$  and  $G_2$  can be written as:

$$G_1 = 1 - \frac{\left[ \frac{\Pi Mb}{W \kappa_0} + \frac{kTd}{W} \left( 1 + \frac{d}{D} \right) - 2 \frac{d}{W} \right]^2}{\Pi^2 \left( \frac{M}{W} \right)^2 \left( \frac{cd + b}{\kappa_0} \right)^2} \tag{4.4}$$

$$G_2 = 1 - \frac{\left[ \frac{\Pi Mb}{W \kappa_0} + \frac{Td}{W} \left( 1 + \frac{d}{D} \right) - 2 \frac{d}{W} \right]^2}{\Pi^2 \left( \frac{M}{W} \right)^2 \left( \frac{cd + b}{\kappa_0} \right)^2}. \tag{4.5}$$

The Appendix lists the method chosen to compute the numbers  $k$  and  $M$  if  $d$ ,  $D$  and  $W$  are given. Using these in [4.4]–[4.5], we have plotted three sets of curves in figures 4–6. In figure 4,  $T = 0$  and we have been able to compare our bounds with the exact volume of  $G$  in eq. [1.12] above due to Kearsley (12). Figures 5 and 6 treat the cases for  $T = 0.25$  and  $T = 0.5$  respectively. The results seem to indicate that if  $D/W = 0.5$ , the bounds come together as  $T$  increases.

Finally, we can derive the limiting values of  $G$  as  $V \rightarrow 0$ , i.e., as the flow occurs due to the pressure gradient alone. If  $V \rightarrow 0$ , then from [3.7]:

$$\left. \begin{aligned} cd + b &\rightarrow CD/2, \\ T\kappa_0 &\rightarrow cD. \end{aligned} \right\} \tag{4.6}$$

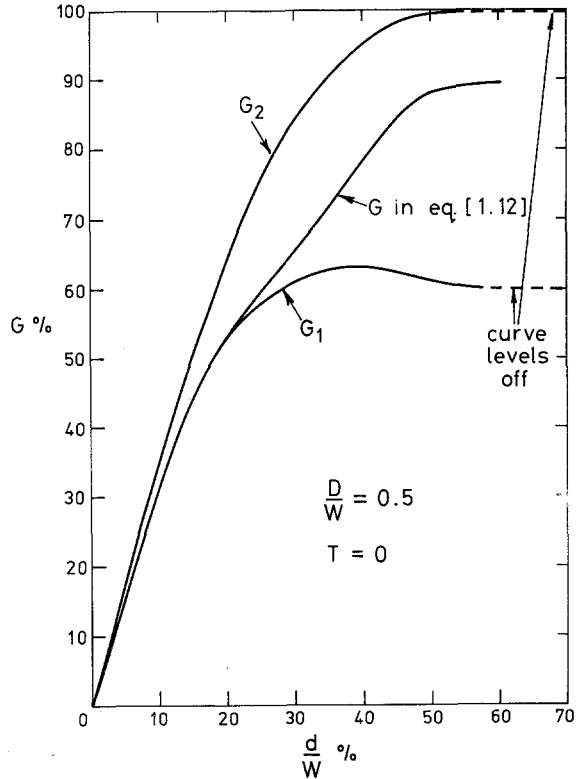


Fig. 4. Upper and lower bounds compared with the exact value of  $G$  for  $c = 0, V > 0, T = 0$

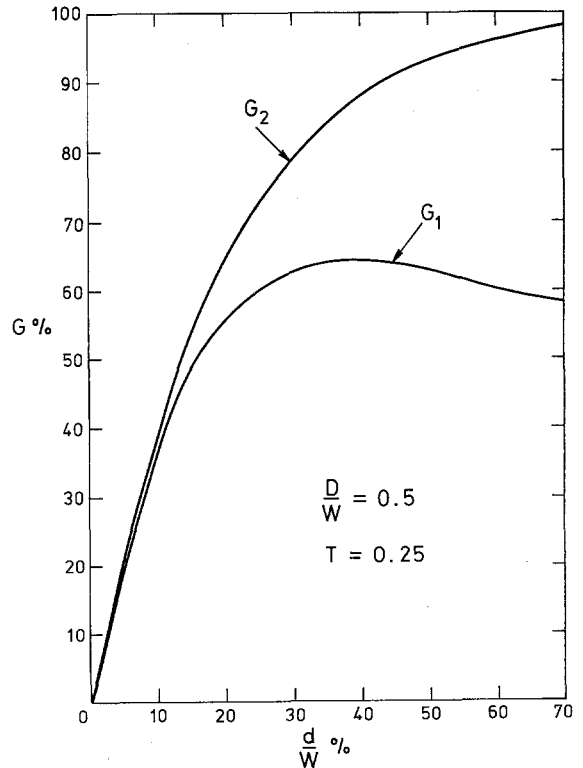


Fig. 5. Upper and lower bounds for  $G, c \neq 0, V > 0, T = 0.25$

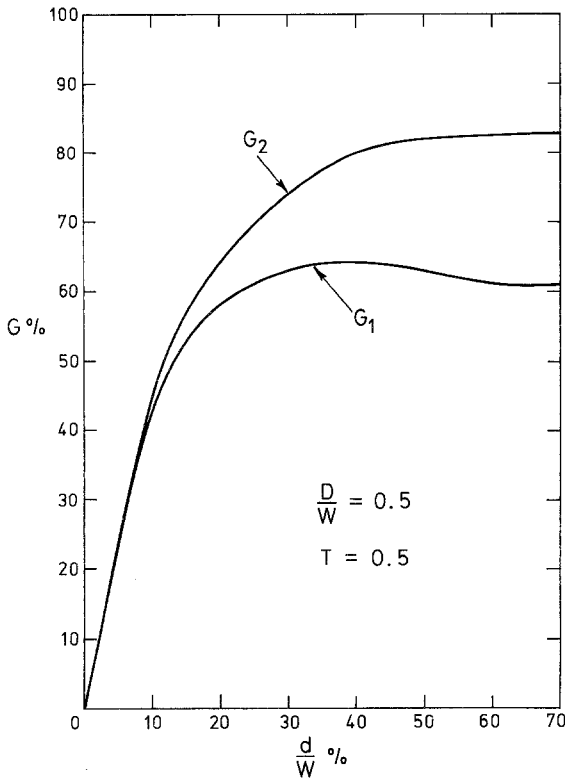


Fig. 6. Upper and lower bounds for  $G$ ,  $c \neq 0$ ,  $V > 0$ ,  $T = 0.5$

Thus, as  $V \rightarrow 0$ ,

$$G_1 \rightarrow 1 - \left( \frac{2kd(1 + d/D)}{\Pi M} \right)^2, \tag{4.7}$$

$$G_2 \rightarrow 1 - \left( \frac{2d(1 + d/D)}{\Pi M} \right)^2. \tag{4.8}$$

These show that  $G_1$  and  $G_2$  become independent of the magnitude of the pressure gradient  $c$ . Of course  $p_e$  will depend on  $c$  through the shear rate  $\kappa_0$  at the wall far away from the slot.

**Appendix**

Given  $d$ ,  $D$  and  $W$ , one obtains (Carter (14)) that:

$$d/W = (2K' - \alpha(D/W))/K \tag{A 1}$$

where  $K = K(k)$  is the complete elliptic integral of the first kind,  $K' = K'(k')$ ,  $k' = (1 - k^2)^{1/2}$ . Eq. [A 1] yields a relationship between  $\alpha$  and  $k$ . Next,

$$\frac{D}{W} = \frac{\pi \operatorname{cn} \alpha}{4 [K \operatorname{cn} \alpha \operatorname{dn} \alpha - K \operatorname{cn} \alpha E(\alpha, k) + \alpha \operatorname{cn} \alpha E(k)]} \tag{A 2}$$

Here  $E(k)$  is the complete elliptic integral of the second kind and  $E(\alpha, k)$  the elliptic integral of the second kind. For all of the above formulae and their meanings, see Hancock (17).

Here, we list the method we have followed to calculate the parameters  $k$  and  $M$  needed in § 4. This procedure is based to a certain extent on the Appendix 3 of Carter (14).

(i) Given  $d/W$  and  $D/W$ , calculate

$$\sigma = \frac{2}{\pi} \left\{ \arctan \left( \frac{2D}{W} \right) - \frac{W}{4D} \ln \left( 1 + \left( \frac{2D}{W} \right)^2 \right) \right\}. \tag{A 3}$$

(ii) Use the elliptic integral of the first kind, i.e.,  $F$  to calculate  $k \operatorname{sn} \alpha$  as follows:

$$\frac{F(\pi/2 - \Theta, \pi/2)}{F(\Theta, \pi/2)} = \frac{2(d + D - \sigma D)}{W}, \tag{A 4}$$

where

$$k \operatorname{sn} \alpha = \sin \Theta. \tag{A 5}$$

(iii) Let

$$\operatorname{sn} \alpha = \sin \varphi \tag{A 6}$$

and calculate, as a first approximation,  $\operatorname{sn} \alpha$  from:

$$\operatorname{sn} \alpha \approx \left[ 1 + \left( \frac{2D}{W} \right)^2 \right]^{-1/2}. \tag{A 7}$$

(iv) Since [A 4] has yielded the exact value of  $k \operatorname{sn} \alpha$  and  $\operatorname{sn} \alpha$  is approximately known from [A 7], we can find a first guess to  $k$ . Use this to find  $K(k)$  and thus  $\alpha$  from

$$\tan \left( \frac{\pi \alpha}{2K} \right) = \frac{W}{2D}. \tag{A 8}$$

The correct relationship between  $k$ ,  $\varphi$  and  $\alpha$  is:

$$\alpha = F(k, \varphi). \tag{A 9}$$

(v) Check if the  $\alpha$ ,  $k$  and  $\operatorname{sn} \alpha$  so determined satisfy [A 1]–[A 2]. If not, assign a new value to  $\operatorname{sn} \alpha$ , recalculate  $k$  and employ [A 9]. Repeat until agreement with [A 1]–[A 2] is obtained to the desired accuracy, say to 3 decimal places.

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*Summary*

The rectilinear flow of a second-order fluid is considered between two infinitely wide and long parallel plates. The bottom plate is at rest and has a longitudinal slot in the direction of the flow, while the top plate moves in the flow direction with a constant speed. Upper and lower bounds for the pressure error are ob-

tained by the use of the maximum principle applied to harmonic functions.

#### Zusammenfassung

Es wird die geradlinige Strömung einer Flüssigkeit zweiter Ordnung zwischen zwei unendlich ausgedehnten parallelen Platten untersucht. Die mit einer rechteckigen, in Strömungsrichtung orientierten Nute versehene Grundplatte befindet sich in Ruhe, wohingegen die glatte Deckplatte sich mit konstanter Geschwindigkeit in Strömungsrichtung bewegt. Untere und obere Schranken für die Abweichung des Druckes infolge der Nute ("pressure error") werden durch Anwendung des Maximumprinzips auf harmonische Funktionen berechnet.

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#### Authors' addresses:

Dr. K. R. Rajagopal  
Department of Applied Mechanics and  
Engineering Science  
University of Michigan  
Ann Arbor, Mich. 48109 (USA)

Dr. R. R. Huilgol  
School of Mathematical Sciences  
Flinders University  
Bedford Park, S.A., 5042 (Australia)